# **MODEL PREDICTIVE CONTROL**

#### LINEAR TIME-VARYING AND NONLINEAR MPC

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#### **COURSE STRUCTURE**

Basic concepts of model predictive control (MPC) and linear MPC

- Linear time-varying and nonlinear MPC
- Quadratic programming (QP) and explicit MPC
- Hybrid MPC
- Stochastic MPC
- Learning-based MPC

## LINEAR TIME-VARYING MODEL PREDICTIVE CONTROL

#### **LPV MODELS**

• Linear Parameter-Varying (LPV) model

$$\begin{cases} x_{k+1} = A(p(t))x_k + B(p(t))u_k + B_v(p(t))v_k \\ y_k = C(p(t))x_k + D_v(p(t))v_k \end{cases}$$

that depends on a vector p(t) of parameters (e.g., ambient conditions)

- The weights in the quadratic performance index can also be LPV
- The resulting optimization problem is still a QP

$$\min_{z} \qquad \frac{1}{2} z' H(p(t)) z + \begin{bmatrix} x(t) \\ r(t) \\ u(t-1) \end{bmatrix}' F(p(t))' z$$
s.t. 
$$G(p(t)) z \leq W(p(t)) + S(p(t)) \begin{bmatrix} x(t) \\ r(t) \\ u(t-1) \end{bmatrix}$$

Contrarily to LTI-MPC, the QP matrices, in general, must be constructed online

#### **LTV MODELS**

• Linear Time-Varying (LTV) model

$$\begin{cases} x_{k+1} = A_k(t)x_k + B_k(t)u_k \\ y_k = C_k(t)x_k \end{cases}$$

- At each time t the model can also change over the prediction horizon  $\boldsymbol{k}$
- Possible measured disturbances are embedded in the model
- Online optimization is still a QP

$$\min_{z} \qquad \frac{1}{2}z'H(t)z + \begin{bmatrix} x(t) \\ r(t) \\ u(t-1) \end{bmatrix}' F(t)'z \\ \text{s.t.} \qquad G(t)z \le W(t) + S(t) \begin{bmatrix} x(t) \\ r(t) \\ u(t-1) \end{bmatrix}$$

• As for LPV-MPC, the QP matrices must be constructed online, in general

• Time-varying process model:

$$\frac{d^3y}{dt^3} + 3\frac{d^2y}{dt^2} + 2\frac{dy}{dt} + (6 + \sin(5t))y = 5\frac{du}{dt} + \left(5 + 2\cos\left(\frac{5}{2}t\right)\right)u$$



• LTI-MPC cannot track the setpoint, LPV-MPC tries to catch up with the time-varying model, LTV-MPC has a preview of future models

>> openExample('mpc/TimeVaryingMPCControlOfATimeVaryingLinearSystemExample')

• Define a sequence of linear models (one per simulation step)

```
Ts = 0.1; % sampling time
Models = tf; ct = 1;
for t = 0:Ts:10
    Models(:,:,ct) = tf([5 5+2*cos(2.5*t)],[1 3 2 6+sin(5*t)]);
    ct = ct + 1;
end
Models = ss(c2d(Models,Ts));
```

• Design a baseline LTI-MPC controller

```
sys = ss(c2d(tf([5 5],[1 3 2 6]),Ts)); % nominal model
p = 3; % prediction horizon
m = 3; % control horizon
mpcobj = mpc(sys,Ts,p,m);
mpcobj.MV = struct('Min',-2,'Max',2); % input constraints
mpcobj.Weights = struct('MV',0,'MVRate',0.01,'Output',1);
```

• Simulate LTV system with LTI-MPC controller

```
for ct = 1:(Tstop/Ts+1)
    real_plant = Models(:,:,ct); % Get the current plant
    y = real_plant.C*x;
    u = mpcmove(mpcobj,xmpc,y,1); % Apply LTI MPC
    x = real_plant.A*x + real_plant.B*u;
end
```

• Simulate LTV system with LPV-MPC controller

```
for ct = 1:(Tstop/Ts+1)
    real_plant = Models(:,:,ct); % Get the current plant
    y = real_plant.C*x;
    u = mpcmoveAdaptive(mpcobj,xmpc,real_plant,nominal,y,1);
    x = real_plant.A*x + real_plant.B*u;
end
```

Simulate LTV system with LTV-MPC controller

• Simulate in Simulink



Simulink block

# need to provide 3D array of future models

#### mpc\_timevarying.mdl

-	
Parameters	
Adaptive MPC Controller mpcob)	
Initial Controller State xmpc	
General Online Features C Prediction Model	others
Linear Time-Varying (LTV) plan	nts (model expects 3-D signals)
Constraints	
Lower MV limits (umin)	Upper MV limits (umax)
Lower OV limits (ymin)	Upper OV limits (ymax)
Custom constraints (E, F, G, S	)
Weights	
OV weights (y.wt)	MV weights (u.wt)
MVRate weights (du.wt)	Slack variable weight (ecr.wt)
Prediction and Control Horizons	
Adjust prediction horizon (p) a	nd control horizon (m) at run time
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## LPV/LTV MPC BASED ON LINEARIZED MODELS

#### LINEARIZING A NONLINEAR MODEL: LPV CASE

• An LPV model can be obtained by linearizing the nonlinear model

$$\begin{cases} \frac{dx_c(t)}{dt} &= f(x_c(t), u_c(t)) \\ y_c(t) &= g(x_c(t)) \end{cases}$$

• At time t, let  $\bar{x}_c(t)$ ,  $\bar{u}_c(t)$  be nominal values, that we assume constant in prediction, and linearize

$$\frac{\frac{d}{d\tau}(x_c(t+\tau)-\bar{x}_c(t)) = \frac{d}{d\tau}(x_c(t+\tau)) \simeq \underbrace{\frac{\partial f}{\partial x}}_{I_{\bar{x}_c(t),\bar{u}_c(t)}} (x_c(t+\tau)-\bar{x}_c(t)) + \underbrace{\frac{\partial f}{\partial u}}_{I_{\bar{x}_c(t),\bar{u}_c(t)}} (u_c(t+\tau)-\bar{u}_c(t)) + \underbrace{f(\bar{x}_c(t),\bar{u}_c(t))}_{B_{vc}(t)} \cdot 1$$

- Convert  $(A_c, [B_c B_{vc}])$  to discrete-time and get prediction model  $(A, [B B_v])$
- Same thing for the output equation to get matrices C and D<sub>v</sub>

#### LINEARIZING A NONLINEAR MODEL: LTV CASE

• LPV/LTV models can be obtained by linearizing a nonlinear model

$$\begin{cases} \frac{dx_c(t)}{dt} &= f(x_c(t), u_c(t)) \\ y_c(t) &= g(x_c(t)) \end{cases}$$

• At time t, consider the **nominal input trajectory** 

$$U = \{ \bar{u}_c(t), \bar{u}_c(t+T_s), \dots, \bar{u}_c(t+(N-1)T_s) \}$$

(example: U = shifted previous optimal sequence or input ref. trajectory)

• Integrate the model from  $\bar{x}_c(t)$  and get nominal state/output trajectories

$$X = \{ \bar{x}_c(t), \bar{x}_c(t+T_s), \dots, \bar{x}_c(t+(N-1)T_s) \}$$
  
$$Y = \{ \bar{y}_c(t), \bar{y}_c(t+T_s), \dots, \bar{y}_c(t+(N-1)T_s) \}$$

• Examples:  $\bar{x}_c(t) = \text{current state / equilibrium state / reference state}$ 

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#### LINEARIZATION AND TIME-DISCRETIZATION

• Linearize the nonlinear model around the nominal states and inputs at each prediction time  $t + kT_s$ , k = 0, ..., N - 1:

• Define  $x \triangleq x_c - \bar{x}_c, u \triangleq u_c - \bar{u}_c, y \triangleq y_c - \bar{y}_c$  and get the linear system

$$\frac{dx}{dt} = A_c(t + kT_s)x + B_c(t + kT_s)u \qquad \qquad y = C(t + kT_s)x$$

• Convert linear model to discrete-time and get matrices  $(A_k(t), B_k(t), C_k(t))$ 

#### LINEARIZATION AND TIME-DISCRETIZATION

• Finally, we have approximated the NL model as the LTV model

$$\begin{pmatrix} \underbrace{x_{k+1}}_{x_c(k+1) - \bar{x}_c(k+1)} = A_k(t) \underbrace{x_c(k) - \bar{x}_c(k)}_{y_c(k) - \bar{y}_c(k)} = C_k(t) \underbrace{x_c(k) - \bar{x}_c(k)}_{x_k} + B_k(t) \underbrace{u_c(k) - \bar{u}_c(k)}_{x_k} \end{pmatrix}$$

(the notation "(k)" is a shortcut for " $(t + kT_s)$ ")

Alternative: while integrating, also compute the sensitivities

$$A_k(t) = \frac{\partial \bar{x}_c(t + (k+1)T_s)}{\partial \bar{x}_c(t + kT_s)}$$
$$B_k(t) = \frac{\partial \bar{x}_c(t + (k+1)T_s)}{\partial \bar{u}_c(t + kT_s)}$$
$$C_k(t) = \frac{\partial \bar{y}_c(t + kT_s)}{\partial \bar{x}_c(t + kT_s)}$$

## INTEGRATION, LINEARIZATION, AND TIME DISCRETIZATION

Forward Euler method

$$\begin{aligned} \bar{x}_c(k+1) &= \bar{x}_c(k) + T_s f(\bar{x}_c(k), \bar{u}_c(k)) \\ A(k) &= I + T_s A_c(k) \\ B(k) &= T_s B_c(k) \end{aligned}$$



Leonhard Paul Euler (1707-1783)

• For improved accuracy we can use smaller integration steps  $\frac{T_s}{N}$ ,  $N \ge 1$ :

L. 
$$x = \bar{x}_c(k), A = I, B = 0$$

2. for n = 1 to N do

• 
$$A \leftarrow \left(I + \frac{T_s}{N} \frac{\partial f}{\partial x_c}(x, \bar{u}_c(k))\right) A$$
  
•  $B \leftarrow \left(I + \frac{T_s}{N} \frac{\partial f}{\partial x_c}(x, \bar{u}_c(k))\right) B + \frac{T_s}{N} \frac{\partial f}{\partial u}(x, \bar{u}_c(k))$   
•  $x \leftarrow x + \frac{T_s}{N} f(x, \bar{u}_c(k))$ 

3. return  $\bar{x}_c(k+1) \approx x$  and matrices A(k) = A, B(k) = B

- Note that integration, linearization, and time-discretization are combined
- See also references in (Gros, Zanon, Quirynen, Bemporad, Diehl, 2020)

#### **EXAMPLE: LPV-MPC OF A NONLINEAR CSTR SYSTEM**

- MPC control of a diabatic continuous stirred tank reactor (CSTR)
- Process model is nonlinear (Seborg, Edgar, Mellichamp, 2004)

$$\begin{aligned} \frac{dC_A}{dt} &= \frac{F}{V}(C_{Af} - C_A) - C_A k_0 e^{-\frac{\Delta E}{RT}} \\ \frac{dT}{dt} &= \frac{F}{V}(T_f - T) + \frac{UA}{\rho C_p V}(T_j - T) - \frac{\Delta H}{\rho C_p} C_A k_0 e^{-\frac{\Delta E}{RT}} \end{aligned}$$



- T: temperature inside the reactor [K] (state)
- $C_A$  : concentration of the reactant in the reactor  $[kgmol/m^3]$  (state)
- $T_j$ : jacket temperature [K] (input)
- $T_f$ : feedstream temperature [K] (measured disturbance)
- $C_{Af}$  : feedstream concentration  $[kgmol/m^3]$  (measured disturbance)
- Objective: manipulate  $T_j$  to regulate  $C_A$  on desired setpoint

```
>> openExample("ampccstr_lpv")
```

(MPC Toolbox)

#### **EXAMPLE: LPV-MPC OF A NONLINEAR CSTR SYSTEM**

• Simulink diagram



#### **EXAMPLE: LPV-MPC OF A NONLINEAR CSTR SYSTEM**

• Closed-loop results









#### **EXAMPLE: LTI-MPC OF A NONLINEAR CSTR SYSTEM**

• Closed-loop results with LTI-MPC, same tuning



#### **EXAMPLE: LTI-MPC OF A NONLINEAR CSTR SYSTEM**

• Closed-loop results









- Goal: Control longitudinal acceleration and steering angle of the vehicle simultaneously for autonomous driving with obstacle avoidance
- Approach: MPC based on a bicycle-like kinematic model of the vehicle in Cartesian coordinates



$$\begin{cases} \dot{x} = v \cos(\theta + \delta) \\ \dot{y} = v \sin(\theta + \delta) \\ \dot{\theta} = \frac{v}{L} \sin(\delta) \end{cases}$$

- $\begin{array}{c|c} (x,y) & \text{Cartesian position of front wheel} \\ \theta & \text{vehicle orientation} \end{array}$ 
  - L vehicle length = 4.5 m

- $v \mid$  velocity at front wheel
  - steering input

• Let  $x_n, y_n, \theta_n, v_n, \delta_n$  be nominal state/input trajectories satisfying

$$\begin{bmatrix} \dot{x}_n \\ \dot{y}_n \\ \dot{\theta}_n \end{bmatrix} = \begin{bmatrix} v_n \cos(\theta_n + \delta_n) \\ v_n \sin(\theta_n + \delta_n) \\ \frac{v_n}{L} \sin(\delta_n) \end{bmatrix}$$

feasible nominal trajectory

• Linearize the model around the nominal trajectory:

$$\begin{bmatrix} \dot{x} \\ \dot{y} \\ \dot{\theta} \end{bmatrix} \approx \begin{bmatrix} \dot{x}_n \\ \dot{y}_n \\ \dot{\theta}_n \end{bmatrix} + A_c \begin{bmatrix} x - x_n \\ y - y_n \\ \theta - \theta_n \end{bmatrix} + B_c \begin{bmatrix} v - v_n \\ \delta - \delta_n \end{bmatrix}$$
 linearized model

where  $A_c$ ,  $B_c$  are the Jacobian matrices

$$A_c = \begin{bmatrix} 0 & 0 & -v_n \sin(\theta_n + \delta_n) \\ 0 & 0 & v_n \cos(\theta_n + \delta_n) \\ 0 & 0 & 0 \end{bmatrix} \quad B_c = \begin{bmatrix} \cos(\theta_n + \delta_n) & -v_n \sin(\theta_n + \delta_n) \\ \sin(\theta_n + \delta_n) & v_n \cos(\theta_n + \delta_n) \\ \frac{1}{L} \sin(\delta_n) & \frac{v_n}{L} \cos(\delta_n) \end{bmatrix}$$

• Use first-order Euler method to discretize model:

$$A = I + T_s A_c, \quad B = T_s B_c, \quad T_s = 50 \,\mathrm{ms}$$

- Constraints on inputs and input variations  $\Delta v_k = v_k v_{k-1}$ ,  $\Delta \delta_k = \delta_k \delta_{k-1}$ :
  - $\begin{array}{ll} -20 \leq v \leq 70 \quad {\rm km/h} & {\rm velocity\ constraint} \\ -45 \leq \delta \leq 45 & {\rm deg} & {\rm steering\ angle} \\ -5 \leq \Delta \delta \leq 5 & {\rm deg} & {\rm steering\ angle\ rate} \end{array}$
- Stage cost to minimize:

$$(x - x_{\rm ref})^2 + (y - y_{\rm ref})^2 + \Delta v^2 + \Delta \delta^2$$

- Prediction horizon: N = 30 (prediction distance =  $NT_s v$ , for example 25 m at 60 km/h)
- Control horizon:  $N_u = 4$
- Preview on reference signals available

• Closed-loop simulation results



• Add position constraint  $y \ge 0 \,\mathrm{m}$ 



## LTV KALMAN FILTER

• Process model = LTV model with noise

$$\begin{array}{lll} x(k+1) &=& A(k)x(k) + B(k)u(k) + G(k)\xi(k) \\ y(k) &=& C(k)x(k) + \zeta(k) \end{array}$$

 $\xi(k) \in \mathbb{R}^q$  = zero-mean white process noise with covariance  $Q(k) \succeq 0$  $\zeta(k) \in \mathbb{R}^p$  = zero-mean white measurement noise with covariance  $R(k) \succ 0$ 

measurement update:

$$M(k) = P(k|k-1)C(k)'[C(k)P(k|k-1)C(k)'+R(k)]^{-1}$$
  

$$\hat{x}(k|k) = \hat{x}(k|k-1) + M(k)(y(k) - C(k)\hat{x}(k|k-1))$$
  

$$P(k|k) = (I - M(k)C(k))P(k|k-1)$$

• time update:

$$\hat{x}(k+1|k) = A(k)\hat{x}(k|k) + B(k)u(k) P(k+1|k) = A(k)P(k|k)A(k)' + G(k)Q(k)G(k)'$$

• Note that here the observer gain L(k) = A(k)M(k)

#### **EXTENDED KALMAN FILTER**

• For state estimation, an Extended Kalman Filter (EKF) can be used based on the same nonlinear model (with additional noise)

$$\begin{aligned} x(k+1) &= f(x(k), u(k), \xi(k)) \\ y(k) &= g(x(k)) + \zeta(k) \end{aligned}$$

measurement update:

• time update:

 $\begin{aligned} \hat{x}(k+1|k) &= f(\hat{x}(k|k), u(k)) \\ A(k) &= \frac{\partial f}{\partial x}(\hat{x}(k|k), u(k), E[\xi(k)]), \ G(k) &= \frac{\partial f}{\partial \xi}(\hat{x}(k|k), u(k), E[\xi(k)]) \\ P(k+1|k) &= A(k)P(k|k)A(k)' + G(k)Q(k)G(k)' \end{aligned}$ 

# **NONLINEAR MODEL PREDICTIVE CONTROL**

• Nonlinear prediction model

$$\begin{cases} x_{k+1} &= f(x_k, u_k) \\ y_k &= g(x_k, u_k) \end{cases}$$

• Nonlinear constraints  $h(x_k, u_k) \leq 0$ 

• Nonlinear performance index min 
$$\ell_N(x_N) + \sum_{k=0}^{N-1} \ell(x_k, u_k)$$

• Optimization problem: nonlinear programming problem (NLP)

$$\begin{array}{ccc} \min_{z} & F(z, x(t)) \\ \text{s.t.} & G(z, x(t)) \leq 0 \\ & H(z, x(t)) = 0 \end{array} \qquad \qquad z = \begin{bmatrix} u_{0} \\ \vdots \\ u_{N-1} \\ \vdots \\ x_{N} \end{bmatrix}$$

#### **NONLINEAR OPTIMIZATION**

- (Nonconvex) NLP is harder to solve than QP
- Convergence to a global optimum may not be guaranteed

- Several NLP solvers exist (such as Sequential Quadratic Programming (SQP)) (Nocedal, Wright, 2006)
- NLP can be useful to deal with strong dynamical nonlinearities and/or nonlinear constraints/costs

• NL-MPC is less used in practice than linear MPC

#### FAST NONLINEAR MPC

- Fast MPC: exploit sensitivity analysis to compensate for the computational delay caused by solving the NLP
- Key idea: pre-solve the NLP between step t-1 and t based on the predicted state  $x^{\ast}(t)=f(x(t-1),u(t-1))$  in background

• Get 
$$u^*(t)$$
 and sensitivity  $\frac{\partial u^*}{\partial x}\Big|_{x^*(t)}$  within sample interval  $[(t-1)T_s, tT_s)$ 

• At time t, get x(t) and compute

$$u(t) = u^*(t) + \frac{\partial u^*}{\partial x}(x(t) - x^*(t))$$

- A.k.a. advanced-step MPC (Zavala, Biegler, 2009)
- Note that still one NLP must be solved within the sample interval

## FROM LTV-MPC TO NONLINEAR MPC

- How to use the LTV-MPC machinery to handle nonlinear MPC?
- Key idea: Solve a sequence of LTV-MPC problems at each time t

(Li, Biegler, 1989) (Lee, Ricker, 1994)

For h = 0 to  $h_{max} - 1$  do:

- 1. Simulate from x(t) with inputs  $U_h$  and get state trajectory  $X_h$
- 2. Linearize around  $(X_h, U_h)$  and discretize in time
- 3. Get  $U_{h+1}^* = \mathbf{QP}$  solution of corresponding LTV-MPC problem
- 4. Line search: find optimal step size  $\alpha_h \in (0, 1]$ ;
- 5. Set  $U_{h+1} = (1 \alpha_h)U_h + \alpha_h U_{h+1}^*$ ;

#### Return solution $U_{h_{\max}}$



• Special case: just solve one iteration with  $\alpha = 1$  (a.k.a. Real-Time Iteration)

(Diehl, Bock, Schloder, Findeisen, Nagy, Allgower, 2002) = LTV-MPC

(Gros, Zanon, Quirynen, Bemporad, Diehl, 2020)

• Example



## **ADVANTAGES OF NONLINEAR MPC**

- Better exploits nonlinear prediction models than LTV-MPC
  - Physics-based models (= white-box models)
  - Machine-learned models (= black-box models, e.g., neural networks)
- Can handle nonlinear inequality constraints (and nonlinear cost functions)

 $g(x) \leq 0$ 







 $g(x_k) + \nabla g(x_k)(x - x_k) \le 0$ 



#### **ODYS EMBEDDED MPC TOOLSET**

• **ODYS Embedded MPC** is a software toolchain for design and deployment of MPC solutions in industrial production



- Support for linear & nonlinear MPC and extended Kalman filtering
- Extremely flexible, all MPC parameters can be changed at runtime (models, cost function, horizons, constraints, ...)
- Integrated with ODYS QP Solver for max speed, low memory footprint, and robustness (also in single precision)
   odys.it/qp
- Library-free C code, MISRA-C 2012 compliant
- Currently used worldwide by several automotive OEMs in R&D and production
- Support for neural networks as prediction models (ODYS Deep Learning)

odys.it/embedded-mpc

#### **ODYS EMBEDDED MPC TOOLSET**

- Models/control specs can be specified either in C-code or MATLAB code
- Built-in automatic integration, discretization, and differentiation of prediction models (optional)
- Efficient handling of sparsity in the prediction models
- User-friendly performance assessment tool for in-depth visualization and detailed analysis of MPC results
- Support for neural networks as prediction models (ODYS Deep Learning)
- Currently used worldwide by several automotive OEMs in R&D and production

See more on: 🔼 (<u>video tutorial</u>) 🔀 (<u>slides</u>)

#### HANDLING DELAYS IN NLMPC

• Nonlinear prediction model with input delay:

$$\begin{cases} x(t+1) &= f(x(t), u(t-\tau)) \\ y(t) &= g(x(t)) \end{cases}$$

$$\underbrace{u(t)}_{u(t-1)} \underbrace{u(t-\tau)}_{t} f() \underbrace{f()}_{y(t)} g() \underbrace{g()}_{y(t)}$$

- Design MPC for delay-free model:  $u(t) = f_{\rm MPC}(\bar{x}(t))$ 

$$\begin{cases} \bar{x}(t+1) &= f(\bar{x}(t), u(t)) \\ \bar{y}(t) &= g(\bar{x}(t)) \end{cases}$$

subject to constraints on u, y

• Simulate the prediction model to estimate the future state:

$$\bar{x}(t) = \hat{x}(t+\tau) = f(x(t+\tau-1), u(t-1)) = \dots = \underbrace{f(f(\dots, f(x(t), u(t-\tau))))}_{t+\tau}$$

only depends on past inputs!

• Compute the MPC control move  $u(t) = f_{MPC}(\hat{x}(t+\tau))$