# **MODEL PREDICTIVE CONTROL**

### **Alberto Bemporad**

http://cse.lab.imtlucca.it/~bemporad/mpc\_course.html



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## **COURSE STRUCTURE**

- Basic concepts of model predictive control (MPC) and linear MPC
- Linear time-varying and nonlinear MPC
- Quadratic programming (QP) and explicit MPC
- Hybrid MPC
- Stochastic MPC
- Learning-based MPC
- Numerical examples:
  - MPC Toolbox for MATLAB (linear/explicit/parameter-varying MPC)
  - Hybrid Toolbox for MATLAB (explicit MPC, hybrid systems)

### **COURSE STRUCTURE**

- For additional background:
  - Linear Systems:

http://cse.lab.imtlucca.it/~bemporad/intro\_control\_course.html

- Numerical Optimization:

http://cse.lab.imtlucca.it/~bemporad/optimization\_course.html

### - Machine Learning:

http://cse.lab.imtlucca.it/~bemporad/ml.html

## **MODEL PREDICTIVE CONTROL: BASIC CONCEPTS**

## **MODEL PREDICTIVE CONTROL (MPC)**



simplified likely Use a dynamical model of the process to predict its future evolution and choose the "best" control action

## **MODEL PREDICTIVE CONTROL**

• MPC problem: find the best control sequence over a future horizon of N steps



t+N+1

t+N

## DAILY-LIFE EXAMPLES OF MPC

• MPC is like playing chess !

Online (event-based) re-planning used in GPS navigation

• You use MPC too when you drive !









## **MPC IN INDUSTRY**

• The MPC concept dates back to the 60's

### Discrete Dynamic Optimization Applied to On-Line Optimal Control

MARSHALL D. RAFAL and WILLIAM F. STEVENS

(Rafal, Stevens, AiChE Journal, 1968)



**А. И. ПРОПОЙ** 



(Propoi, 1963)

• MPC used in the process industries since the 80's

(Qin, Badgewell, 2003) (Bauer, Craig, 2008)

### Today APC (advanced process control) = MPC



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Area	Aspen Technology	Honeywell Hi-Spec	Adersa <sup>b</sup>	Invensys	SGS <sup>c</sup>	Total
Refining	1200	480	280	25		1985
Petrochemicals	450	80	_	20		550
Chemicals	100	20	3	21		144
Pulp and paper	18	50	_	_		68
Air & Gas		10	_	_		10
Utility		10	_	4		14
Mining/Metallurgy	8	6	7	16		37
Food Processing		_	41	10		51
Polymer	17	_	_	_		17
Furnaces		_	42	3		45
Aerospace/Defense		_	13	_		13
Automotive		_	7	_		7
Unclassified	40	40	1045	26	450	1601
Total	1833	696	1438	125	450	4542
First App.	DMC:1985	PCT:1984	IDCOM:1973			
	IDCOM-M:1987 OPC:1987	RMPCT:1991	HIECON:1986	1984	1985	
Largest App.	$603 \times 283$	$225 \times 85$	_	$31 \times 12$	_	

• Industrial survey of MPC applications conducted in mid 1999

### Estimates based on vendor survey

## MPC IN INDUSTRY

Economic assessment of Advanced Process Control (APC)

Petrochemical Chemicals Petroleum refining Mineralsprocessing Oil & Gas Power & utilities Pulp & paper Industrial gases Coal products D Suppliers Users Other 40% 60% 80% 100% 0% 20%

participants of APC survey by industry (worldwide)

Frequently Rarely Never

Standard

Don't know

### 20%Industrial use of APC methods: survey results

0%

Model predictive control

Linear programming (LP)

Dead-time compensation Statistical process control Neural networks based control Expert system based control Fuzzy logic control Internal model control (IMC) Adaptive / selftuning control Directsynthesis (DS)

Nonlinear control algorithms or models

Constraint control

Split-range control





### (Bauer, Craig, 2008)

### • Impact of advanced control technologies in industry

TABLE 1 A list of the survey results in order of industry impact as perceived by the committee members.

Rank and Technology	High-Impact Ratings	Low- or No-Impact Ratings
PID control	100%	0%
Model predictive control	78%	9%
System identification	61%	9%
Process data analytics	61%	17%
Soft sensing	52%	22%
Fault detection and identification	50%	18%
Decentralized and/or coordinated control	48%	30%
Intelligent control	35%	30%
Discrete-event systems	23%	32%
Nonlinear control	22%	35%
Adaptive control	17%	43%
Robust control	13%	43%
Hybrid dynamical systems	13%	43%

## **MPC IN INDUSTRY**

### Table 2

The percentage of survey respondents indicating whether a control technology had demonstrated ("Current Impact") or was likely to demonstrate over the next five years ("Future Impact") high impact in practice.

	Current Impact	Future Impact
Control Technology	%High	%High
PID control	91%	78%
System Identification	65%	72%
Estimation and filtering	64%	63%
Model-predictive control	62%	85%
Process data analytics	51%	70%
Fault detection and identification	48%	78%
Decentralized and/or coordinated control	29%	54%
Robust control	26%	42%
Intelligent control	24%	59%
Discrete-event systems	24%	39%
Nonlinear control	21%	42%
Adaptive control	18%	44%
Repetitive control	12%	17%
Hybrid dynamical systems	11%	33%
Other advanced control technology	11%	25%
Game theory	5%	17%

(Samad et al., 2020)

"As can be observed, MPC is clearly considered more impactful, and likely to be more impactful, vis-à-vis other control technologies, especially those that can be considered the "crown jewels" of control theory - robust control, adaptive control, and nonlinear control."

## **TYPICAL USE OF MPC**

strategic planner



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## **MPC OF AUTOMOTIVE SYSTEMS**

(Bemporad, Bernardini, Borrelli, Cimini, Di Cairano, Esen, Giorgetti, Graf-Plessen, Hrovat, Kolmanovsky Levijoki, Livshiz, Long, Pattipati, Ripaccioli, Trimboli, Tseng, Verdejo, Yanakiev, ..., 2001-present)

### Powertrain

engine control, magnetic actuators, robotized gearbox, power MGT in HEVs, cabin heat control, electrical motors

### Vehicle dynamics

traction control, active steering, semiactive suspensions, autonomous driving

Ford Motor Company Jaguar DENSO Automotive Fiat General Motors



### Most automotive OEMs are looking into MPC solutions today

### **SYSTEMS**

(Graf Plessen, Bernardini, Esen, Bemporad, 2018)

- Coordinate torque request and steering to achieve safe and comfortable autonomous driving with no collisions
- MPC combines path planning, path tracking, and obstacle avoidance
- Stochastic prediction models used to account for uncertainty (other vehicles/pedestrians, driver's requests)





## **MPC OF GASOLINE TURBOCHARGED ENGINES**

• Control throttle, wastegate, intake & exhaust cams to make engine torque track set-points, with max efficiency and satisfying constraints



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engine operating at low pressure (66 kPa)

## SUPERVISORY MPC OF POWERTRAIN WITH CVT

- Coordinate engine torque request and continuously variable transmission (CVT) ratio to improve fuel economy and drivability
- Real-time MPC is able to take into account **coupled dynamics** and **constraints**, optimizing performance also during transients



## **MPC IN AUTOMOTIVE PRODUCTION**

**ODYS** real-time embedded optimization and MPC software is currently running on **3+ million vehicles** worldwide

• Multivariable system, 4 inputs, 4 outputs. QP solved in real time on ECU

(Bemporad, Bernardini, Long, Verdejo, 2018)

• Supervisory MPC for powertrain control also in production since 2018

(Bemporad, Bernardini, Livshiz, Pattipati, 2018)

### First known mass production of MPC in the automotive industry

### and more are underway...

http://www.odys.it/odys-and-gm-bring-online-mpc-to-production



### **AEROSPACE APPLICATIONS OF MPC**

• MPC capabilities explored in space applications





(Bemporad, Rocchi, 2011)

(Pascucci, Bennani, Bemporad, 2016)

(Krenn et. al., 2012)

• Online convex optimization (≈ MPC) is used by SpaceX to land reusable rockets (Blackmore, 2016)

### **PRESS RELEASE**

Pratt & Whitney's F135 Advanced Multi-Variable Control Team Receives UTC's Prestigious George Mead Award for Outstanding Engineering Accomplishment

### EAST HARTFORD, CONN., THURSDAL MAY 27, 2010



Pratt & Whitney engineers Louis Celiberti, Timothy Crowley, James Fuller and Cary Powell won the George Mead Award – United Technologies Corp.'s highest award for outstanding engineering achievement – for their pioneering work in developing the world's first advanced multi-variable control (AMVC) design for the only engine that powers the F-35 Lightning II flight test program. Pratt & Whitney is a United Technologies Corp. (NYSE:UTX) company.

The AWVC, which uses a proprietary model predictive control methodology, is the most technically advanced propulsion system control ever produced by the aerospace industry, demonstrating the highest pilot rating for flight performance and providing independent control of vertical thrust and pitch from five sources. This innovative and industry-leading advanced design is protected with five broad patents for Pratt & Whitney and UTC, and is the new standard for propulsion system control for Pratt & Whitney military and commercial engines.





http://www.pw.utc.com/Press/Story/20100527-0100/2010

### **MPC FOR SMART ELECTRICITY GRIDS**

(Patrinos, Trimboli, Bemporad, 2011)



Dispatch power in smart distribution grids, trade energy on energy markets

Challenges: account for dynamics, network topology, physical constraints, and stochasticity (of renewable energy, demand, electricity prices) FP7-ICT project "E-PRICE - Price-based Control of Electrical Power Systems" (2010-2013)

## **MPC OF DRINKING WATER NETWORKS**

(Sampathirao, Sopasakis, Bemporad, Patrinos, 2017)



Drinking water network of Barcelona:

63 tanks 114 controlled flows 17 mixing nodes



- $\approx$ **5% savings** on energy costs w.r.t. current practice
- Demand and minimum pressure requirements met, smooth control actions
- Computation time: ≈20 s on NVIDIA Tesla 2075 CUDA (sample time = 1 hr) FP7-ICT project "EFFINET - Efficient Integrated Real-time Monitoring and Control of Drinking Water Networks" (2012-2015)

## **MPC FOR DYNAMIC HEDGING OF FINANCIAL OPTIONS**

(Bemporad, Bellucci, Gabbriellini, Quantitative Finance, 2014)

- Goal: find a dynamic hedging policy of a portfolio replicating a synthetic option, so to minimize risk that payoff 
  portfolio wealth at expiration date
- A simple linear stochastic model describes the dynamics of portfolio wealth
- Stochastic MPC results:



### **MPC RESEARCH IS DRIVEN BY APPLICATIONS**

• Process control $\rightarrow$ <b>linear</b> MPC (some <b>nonlinear</b> too)	1970-2000
• Automotive control $\rightarrow$ <b>explicit</b> , <b>hybrid</b> MPC	2001-2010
• Aerospace systems and UAVs $\rightarrow$ linear time-varying MPC	>2005
<ul> <li>Information and Communication Technologies (ICT) (wireless nets, cloud) → distributed/decentralized MPC</li> </ul>	>2005
• Energy, finance, automotive, water $\rightarrow$ stochastic MPC	>2010
• Industrial production $\rightarrow$ <b>embedded optimization</b> solvers for MPC	>2010
• Machine learning $\rightarrow$ <b>data-driven</b> MPC	today

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## **MPC DESIGN FLOW**



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### **MPC TOOLBOXES**

- MPC Toolbox (The Mathworks, Inc.): (Bemporad, Ricker, Morari, 1998-today)
  - Part of Mathworks' official toolbox distribution
  - All written in MATLAB code
  - Great for education and research
- Hybrid Toolbox:
  - Free download: http://cse.lab.imtlucca.it/~bemporad/hybrid/toolbox
  - Great for research and education
- ODYS Embedded MPC Toolset:
  - Very flexible MPC design and seamless integration in production
  - Real-time MPC code and QP solver written in plain C
  - Support for nonlinear models and deep learning
  - Designed and adopted for <u>industrial production</u>

11,500+ downloads 1.5 downloads/day

(Bemporad, 2003-today)

odys.it/embedded-mpc





## **BENEFITS OF MPC**

- Long history (decades) of success of MPC in industry
- MPC is a universal control methodology:
  - to coordinate multiple inputs/outputs, arbitrary models (linear, nonlinear, ...)
  - to optimize performance under constraints
  - intuitive to design, easy to calibrate and reconfigure = short development time
- MPC is a mature technology also in fast-sampling applications (e.g. automotive)
  - modern ECUs can solve MPC problems in real-time
  - advanced MPC software tools are available for design/calibration/deployment

### Ready to learn how MPC works?

## **BASICS OF CONSTRAINED OPTIMIZATION**

### See more in "Numerical Optimization" course

http://cse.lab.imtlucca.it/~bemporad/optimization\_course.html

### MATHEMATICAL PROGRAMMING



$$x = \begin{bmatrix} x_1 \\ \vdots \\ x_n \end{bmatrix}, \quad f(x) = f(x_1, x_2, \dots, x_n), \quad g(x) = \begin{bmatrix} g_1(x_1, x_2, \dots, x_n) \\ \vdots \\ g_m(x_1, x_2, \dots, x_n) \end{bmatrix}$$

In general, the problem is difficult to solve

use software tools

### **OPTIMIZATION SOFTWARE**

• Comparison on benchmark problems:

http://plato.la.asu.edu/bench.html

• Taxonomy of many solvers for different classes of optimization problems:

http://www.neos-guide.org

• NEOS server for remotely solving optimization problems:

http://www.neos-server.org

• Good open-source optimization software:

http://www.coin-or.org/

• GitHub , MATLAB Central , Google , ...

### **CONVEX SETS**

• A set  $S \subseteq \mathbb{R}^n$  is convex if for all  $x_1, x_2 \in S$ 

$$\lambda x_1 + (1 - \lambda) x_2 \in S, \, \forall \lambda \in [0, 1]$$



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### **CONVEX FUNCTIONS**

• A function  $f:S \to \mathbb{R}$  is a **convex function** if S is convex and

 $f(\lambda x_1 + (1 - \lambda)x_2) \le \lambda f(x_1) + (1 - \lambda)f(x_2)$  $\forall x_1, x_2 \in S, \ \lambda \in [0, 1]$ 

Jensen's inequality



## **CONVEX OPTIMIZATION PROBLEM**

### The optimization problem

 $\begin{array}{ll} \min & f(x) \\ \text{s.t.} & x \in S \end{array}$ 



is a **convex optimization problem** if S is a convex set and  $f: S \to \mathbb{R}$  is a convex function



- Often S is defined by linear equality constraints Ax = b and convex inequality constraints g(x) ≤ 0, g : ℝ<sup>n</sup> → ℝ<sup>m</sup> convex
- Every local solution is also a global one (we will see this later)
- Efficient solution algorithms exist
- Often occurring in many problems in engineering, economics, and science Excellent textbook: "Convex Optimization" (Boyd, Vandenberghe, 2002)

## POLYHEDRA

- Convex polyhedron = intersection of a finite set of half-spaces of ℝ<sup>n</sup>
- Convex **polytope** = bounded convex polyhedron
- Hyperplane (H-)representation:

 $P = \{ x \in \mathbb{R}^n : Ax \le b \}$ 

• Vertex (V-)representation:

$$P = \{x \in \mathbb{R}^n : x = \sum_{i=1}^q \alpha_i v_i + \sum_{j=1}^p \beta_j r_j\}$$
$$\alpha_i, \beta_j \ge 0, \sum_{i=1}^q \alpha_i = 1, v_i, r_j \in \mathbb{R}^n$$

when q = 0 the polyhedron is a cone

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**Convex hull** = transformation from V- to H-representation

Vertex enumeration =

transformation from H- to V-representation

 $v_i$  = vertex,  $r_j$  = extreme ray

### LINEAR PROGRAMMING

• Linear programming (LP) problem:

 $\begin{array}{ll} \min & c'x \\ \text{s.t.} & Ax \leq b, \, x \in \mathbb{R}^n \\ & Ex = f \end{array}$ 

• LP in standard form:





George Dantzig (1914–2005)

- Conversion to standard form:
  - 1. introduce slack variables

$$\sum_{j=1}^{n} a_{ij}x_j \leq b_i \Rightarrow \sum_{j=1}^{n} a_{ij}x_j + s_i = b_i, \, s_i \geq 0$$

min

s.t.

2. split positive and negative part of x

$$\begin{cases} \sum_{j=1}^{n} a_{ij}x_j + s_i = b_i \\ x_j \text{ free, } s_i \ge 0 \end{cases} \Rightarrow \begin{cases} \sum_{j=1}^{n} a_{ij}(x_j^+ - x_j^-) + s_i = b_i \\ x_j^+, x_j^-, s_i \ge 0 \end{cases}$$

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## LINEAR PROGRAMMING (LP)

• Converting maximization to minimization

 $\max_x c'x = -(\min_x - c'x) \qquad (\text{more generally: } \max_x f(x) = -\min_x \{-f(x)\})$ 

• Equalities to double inequalities (not recommended)

$$\sum_{j=1}^{n} a_{ij} x_j = b_i \Rightarrow \begin{cases} \sum_{j=1}^{n} a_{ij} x_j \le b_i \\ \sum_{j=1}^{n} a_{ij} x_j \ge b_i \end{cases}$$

• Change direction of an inequality

$$\sum_{j=1}^{n} a_{ij} x_j \ge b_i \implies \sum_{j=1}^{n} -a_{ij} x_j \le -b_i$$

An LP can be always formulated using "min" and " $\leq$ "
# **QUADRATIC PROGRAMMING (QP)**

• Quadratic programming (QP) problem:

$$\begin{array}{ll} \min & \frac{1}{2}x'Qx + c'x \\ \text{s.t.} & Ax \leq b, \ x \in \mathbb{R}^n \\ & Ex = f \end{array}$$



- Convex optimization problem if  $Q \succeq 0$  (Q = positive semidefinite matrix) <sup>1</sup>
- Without loss of generality, we can assume Q = Q':

$$\frac{1}{2}x'Qx = \frac{1}{2}x'(\frac{Q+Q'}{2} + \frac{Q-Q'}{2})x = \frac{1}{2}x'(\frac{Q+Q'}{2})x + \frac{1}{4}x'Qx - \frac{1}{4}(x'Q'x)'$$

$$= \frac{1}{2}x'(\frac{Q+Q'}{2})x$$

• Hard problem if  $Q \not\succeq 0$  (Q = indefinite matrix)

<sup>1</sup> A matrix  $P \in \mathbb{R}^{n \times n}$  is positive semidefinite  $(P \succeq 0)$  if  $x'Px \ge 0$  for all x. It is positive definite  $(P \succ 0)$  if in addition x'Px > 0 for all  $x \ne 0$ . It is negative (semi)definite  $(P \prec 0, P \preceq 0)$  if -P is positive (semi)definite. It is indefinite otherwise.

#### MIXED-INTEGER PROGRAMMING (MIP)

$$\begin{array}{ll} \min & c'x \\ \text{s.t.} & Ax \leq b, \, x = \left[ \begin{smallmatrix} x_c \\ x_b \end{smallmatrix} \right] \\ & x_c \in \mathbb{R}^{n_c}, \, x_b \in \{0,1\}^{n_b} \end{array}$$

$$\begin{array}{ll} \min & \frac{1}{2}x'Qx + c'x \\ \text{s.t.} & Ax \leq b, \ x = \left[ \begin{smallmatrix} x_c \\ x_b \end{smallmatrix} \right] \\ & x_c \in \mathbb{R}^{n_c}, \ x_b \in \{0,1\}^{n_b} \end{array}$$

mixed-integer quadratic program (MIQP)

- Some variables are real, some are binary (0/1)
- MILP and MIQP are  $\mathcal{NP}$ -hard problems, in general
- Many good solvers are available (CPLEX, Gurobi, GLPK, FICO Xpress, CBC, ...) For comparisons see http://plato.la.asu.edu/bench.html

# **MODELING LANGUAGES FOR OPTIMIZATION PROBLEMS**

- AMPL (A Modeling Language for Mathematical Programming) most used modeling language, supports several solvers
- GAMS (General Algebraic Modeling System) is one of the first modeling languages
- GNU MathProg a subset of AMPL associated with the free package GLPK (GNU Linear Programming Kit)
- YALMIP MATLAB-based modeling language
- CVX (CVXPY) Modeling language for convex problems in MATLAB ( python )

# **MODELING LANGUAGES FOR OPTIMIZATION PROBLEMS**

- CASADI + IPOPT Nonlinear modeling + automatic differentiation, nonlinear programming solver (MATLAB, python, C++)
- Optimization Toolbox' modeling language (part of MATLAB since R2017b)
- **PYOMO Python**-based modeling language
- GEKKO 📌 python-based mixed-integer nonlinear modeling language
- PYTHON-MIP python-based modeling language for mixed-integer linear programming
- JuMP A modeling language for linear, quadratic, and nonlinear constrained optimization problems embedded in **julia**

# LINEAR MPC

# LINEAR MPC - UNCONSTRAINED CASE

Linear prediction model

$$\begin{cases} x_{k+1} = Ax_k + Bu_k \\ y_k = Cx_k \end{cases} \qquad \begin{array}{c} x \in \mathbb{R}^n \\ u \in \mathbb{R}^m \\ y \in \mathbb{R}^p \end{cases}$$

Notation:  

$$x_0 = x(t)$$
  
 $x_k = x(t+k|t)$   
 $u_k = u(t+k|t)$ 

• Relation between input and states:  $x_k = A^k x_0 + \sum_{j=0}^{k-1} A^j B u_{k-1-j}$ 

Performance index

$$J(z, x_0) = x'_N P x_N + \sum_{k=0}^{N-1} x'_k Q x_k + u'_k R u_k \quad \begin{cases} R &= R' \succ 0 \\ Q &= Q' \succeq 0 \\ P &= P' \succeq 0 \end{cases} \quad z = \begin{bmatrix} u_0 \\ u_1 \\ \vdots \\ u_{N-1} \end{bmatrix}$$

• Goal: find the sequence  $z^*$  that minimizes  $J(z, x_0)$ , i.e., that steers the state x to the origin optimally

#### **COMPUTATION OF COST FUNCTION**

$$J(z, x_{0}) = x_{0}'Qx_{0} + \begin{bmatrix} x_{1} \\ x_{2} \\ \vdots \\ x_{N-1} \\ x_{N} \end{bmatrix}' \underbrace{\begin{bmatrix} Q & 0 & 0 & \dots & 0 \\ 0 & Q & 0 & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots & \vdots \\ 0 & \dots & 0 & Q & 0 \\ 0 & 0 & \dots & 0 & P \end{bmatrix}}_{\begin{bmatrix} x_{1} \\ x_{2} \\ \vdots \\ x_{N-1} \end{bmatrix}' + \begin{bmatrix} u_{0} \\ u_{1} \\ \vdots \\ u_{N-1} \end{bmatrix}' \underbrace{\begin{bmatrix} R & 0 & \dots & 0 \\ 0 & R & \dots & 0 \\ 0 & R & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & \dots & 0 & R \end{bmatrix}}_{\bar{R}} \begin{bmatrix} u_{0} \\ u_{1} \\ \vdots \\ u_{N-1} \end{bmatrix} + \underbrace{\begin{bmatrix} A^{2} \\ A^{2} \\ \vdots \\ A^{N} \end{bmatrix}}_{\bar{T}} x_{0}$$
$$J(z, x_{0}) = (\bar{S}z + \bar{T}x_{0})'\bar{Q}(\bar{S}z + \bar{T}x_{0}) + z'\bar{R}z + x'_{0}Qx_{0} \\ = \frac{1}{2}z' \underbrace{2(\bar{R} + \bar{S}'\bar{Q}\bar{S})}_{H} z + x'_{0} \underbrace{2\bar{T}'\bar{Q}\bar{S}}_{F'} z + \frac{1}{2}x'_{0} \underbrace{2(Q + \bar{T}'\bar{Q}\bar{T})}_{Y} x_{0}$$

#### LINEAR MPC - UNCONSTRAINED CASE

$$J(z, x_0) = \frac{1}{2}z'Hz + x'_0F'z + \frac{1}{2}x'_0Yx_0 \qquad z = \begin{bmatrix} u_0 \\ u_1 \\ \vdots \\ u_{N-1} \end{bmatrix} \text{ condensed form of MPC}$$

 $\nabla I(z, x_2) = Hz + Ex_2 = 0$ 

• The optimum is obtained by zeroing the gradient

and hence 
$$z^* = \begin{bmatrix} u_0^* \\ u_1^* \\ \vdots \\ u_{N-1}^* \end{bmatrix} = -H^{-1}Fx_0$$
 ("batch" solution)

- Alternative #1: find z\* via dynamic programming (Riccati iterations)
- Alternative #2: keep also  $x_1, \ldots, x_N$  as optimization variables and the equality constraints  $x_{k+1} = Ax_k + Bu_k$  (non-condensed form, which is very sparse)

#### **UNCONSTRAINED LINEAR MPC ALGORITHM**

@ each sampling step t:



Minimize quadratic function (no constraints)

$$\min_{z} f(z) = \frac{1}{2} z' H z + x'(t) F' z \qquad z = \begin{bmatrix} u_{0} \\ u_{1} \\ \vdots \\ u_{N-1} \end{bmatrix}$$

• solution:  $\nabla f(z) = Hz + Fx(t) = 0 \Rightarrow z^* = -H^{-1}Fx(t)$ 

$$u(t) = -\begin{bmatrix} I & 0 & \dots & 0 \end{bmatrix} H^{-1} F \mathbf{x}(t) = K \mathbf{x}(t)$$

#### unconstrained linear MPC = linear state-feedback!

# **CONSTRAINED LINEAR MPC**

• Linear prediction model: 
$$\begin{cases} x_{k+1} = Ax_k + Bu_k & x \in \mathbb{R}^n \\ y_k = Cx_k & u \in \mathbb{R}^m \\ u \in \mathbb{R}^p \end{cases}$$

• Constraints to enforce:

 $\begin{cases} u_{\min} \le u(t) \le u_{\max} & u_{\min}, u_{\max} \in \mathbb{R}^m \\ y_{\min} \le y(t) \le y_{\max} & y_{\min}, y_{\max} \in \mathbb{R}^p \end{cases}$ 

• Constrained optimal control problem (quadratic performance index):

$$\min_{z} \quad x'_{N} P x_{N} + \sum_{k=0}^{N-1} x'_{k} Q x_{k} + u'_{k} R u_{k} \\ \text{s.t.} \quad u_{\min} \leq u_{k} \leq u_{\max}, \ k = 0, \dots, N-1 \\ y_{\min} \leq y_{k} \leq y_{\max}, \ k = 1, \dots, N \\ \end{array} \right| \begin{array}{l} R \quad = \quad R' \succ 0 \\ Q \quad = \quad Q' \succeq 0 \\ P \quad = \quad P' \succeq 0 \\ R \quad = \quad R' \succ 0 \\ Q \quad = \quad Q' \succeq 0 \\ P \quad = \quad P' \succeq 0 \\ \end{array} \right|$$

# **CONSTRAINED LINEAR MPC**

• Linear prediction model: 
$$x_k = A^k x_0 + \sum_{i=0}^{k-1} A^i B u_{k-1-i}$$

• Optimization problem (condensed form):

$$V(x_0) = \frac{1}{2}x'_0Yx_0 + \min_{z} \quad \frac{1}{2}z'Hz + x'_0F'z \quad \text{(quadratic objective)}$$
  
s.t.  $Gz \le W + Sx_0$  (linear constraints)

#### convex Quadratic Program (QP)

• 
$$z = \begin{bmatrix} u_0 \\ u_1 \\ \vdots \\ u_{N-1} \end{bmatrix} \in \mathbb{R}^{Nm}$$
 is the optimization vector

$$G_2 \leq W + S_2(t)$$

 H = H' ≻ 0, and H, F, Y, G, W, S depend on weights Q, R, P upper and lower bounds u<sub>min</sub>, u<sub>max</sub>, y<sub>min</sub>, y<sub>max</sub> and model matrices A, B, C.

# **COMPUTATION OF CONSTRAINT MATRICES**

• Input constraints 
$$u_{\min} \le u_k \le u_{\max}, \ k = 0, \dots, N-1$$

$$\left\{\begin{array}{ccccc} u_{k} &\leq & u_{\max} \\ -u_{k} &\leq & -u_{\min} \end{array}\right\} \longrightarrow \left[\begin{array}{ccccc} 1 & 0 & \dots & 0 \\ 0 & 1 & \dots & 0 \\ \vdots & & \ddots & \vdots \\ 0 & \dots & 0 & 1 \\ -1 & 0 & \dots & 0 \\ 0 & -1 & \dots & 0 \\ \vdots & & \ddots & \vdots \\ 0 & \dots & 0 & -1 \end{array}\right] z \leq \left[\begin{array}{c} u_{\max} \\ u_{\max} \\ \vdots \\ u_{\max} \\ -u_{\min} \\ \vdots \\ -u_{\min} \\ \vdots \\ -u_{\min} \end{array}\right] \qquad z = \left[\begin{array}{c} u_{0} \\ u_{1} \\ \vdots \\ u_{N-1} \end{array}\right]$$

• Output constraints 
$$y_k = CA^k x_0 + \sum_{i=0}^{k-1} CA^i Bu_{k-1-i} \le y_{\max}, \ k = 1, \dots, N$$

$$\begin{bmatrix} CB & 0 & \dots & 0\\ CAB & CB & \dots & 0\\ \vdots & & & \vdots\\ CA^{N-1}B & \dots & CAB & CB \end{bmatrix} z \leq \begin{bmatrix} y_{\max}\\ y_{\max}\\ \vdots\\ y_{\max} \end{bmatrix} - \begin{bmatrix} CA\\ CA^2\\ \vdots\\ CA^N \end{bmatrix} x_0$$

# LINEAR MPC ALGORITHM



@ each sampling step t:

• Measure (or estimate) the current state x(t)

• Get the solution 
$$z^* = \begin{bmatrix} u_0^* \\ u_1^* \\ \vdots \\ u_{N-1}^* \end{bmatrix}$$
 of the QP 
$$\begin{cases} \min_{z} \quad \frac{1}{2}z'Hz + \overbrace{x'(t)F'z}^{\text{feedback}} \\ \text{s.t.} \quad Gz \leq W + S \underbrace{x(t)}_{\text{feedback}} \end{cases}$$

- Apply only  $u(t) = u_0^*,$  discarding the remaining optimal inputs  $u_1^*, \ldots, u_{N-1}^*$ 

• System: 
$$x_2(t) = x_2(0) + \sum_{j=0}^{t-1} u(j), y(t) = x_1(0) + \sum_{j=0}^{t-1} x_2(j)$$

• Sample time:  $T_s = 1 \text{ s}$ 

• State-space realization: 
$$\begin{cases} x(t+1) &= \begin{bmatrix} 1 & 1 \\ 0 & 1 \end{bmatrix} x(t) + \begin{bmatrix} 0 \\ 1 \end{bmatrix} u(t) \\ y(t) &= \begin{bmatrix} 1 & 0 \end{bmatrix} x(t) \end{cases}$$

• Constraints: 
$$-1 \le u(t) \le 1$$

• Performance index: 
$$\min\left(\sum_{k=0}^{1} y_k^2 + \frac{1}{10} u_k^2\right) + x'_N \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix} x_N, \quad N = 2$$

QP matrices:

 $\begin{array}{l} \text{COSt:} \quad \frac{1}{2}z'Hz + x'(t)F'z + \frac{1}{2}x'(t)Yx(t) \\ \text{CONSTRAINTS:} \quad Gz \leq W + Sx(t) \end{array} \qquad \begin{array}{l} H = \begin{bmatrix} 4.2 & 2\\ 2 & 2.2 \end{bmatrix}, \ F = \begin{bmatrix} 2 & 6\\ 0 & 2 \end{bmatrix} \\ Y = \begin{bmatrix} 4 & 6\\ 6 & 12 \end{bmatrix}, \ G = \begin{bmatrix} 1 & 0\\ -1 & 0\\ 0 & -1 \end{bmatrix} \\ W = \begin{bmatrix} 1\\ 1\\ 1\\ 1 \end{bmatrix}, \ S = \begin{bmatrix} 0 & 0\\ 0 & 0\\ 0 & 0 \end{bmatrix}$ 



go to demo linear/doubleint.m(Hybrid Toolbox)
(see also mpcdoubleint.m in MPC Toolbox)

• Add constraint on second state at prediction time t + 1:

$$x_{2,k} \ge -1, \ k = 1$$

• New QP matrices:

$$H = \begin{bmatrix} 4.2 & 2\\ 2 & 2.2 \end{bmatrix}, F = \begin{bmatrix} 2 & 6\\ 0 & 2 \end{bmatrix}, Y = \begin{bmatrix} 4 & 6\\ 6 & 12 \end{bmatrix}$$
$$G = \begin{bmatrix} -1 & 0\\ 1 & 0\\ -1 & 0\\ 0 & -1 \end{bmatrix}, W = \begin{bmatrix} 1\\ 1\\ 1\\ 1\\ 1 \end{bmatrix}, S = \begin{bmatrix} 0 & 1\\ 0 & 0\\ 0 & 0\\ 0 & 0 \end{bmatrix}$$



• State constraint  $x_2(t) \ge -1$  is satisfied

# LINEAR MPC - TRACKING

- Objective: make the output y(t) track a reference signal r(t)
- Let us parameterize the problem using the input increments

$$\Delta u(t) = u(t) - u(t-1)$$

- As  $u(t)=u(t-1)+\Delta u(t)$  we need to extend the system with a new state  $x_u(t)=u(t-1)$ 

$$\begin{cases} x(t+1) = Ax(t) + Bu(t-1) + B\Delta u(t) \\ x_u(t+1) = x_u(t) + \Delta u(t) \end{cases}$$

$$\begin{cases} \begin{bmatrix} x(t+1) \\ x_u(t+1) \end{bmatrix} = \begin{bmatrix} A & B \\ 0 & I \end{bmatrix} \begin{bmatrix} x(t) \\ x_u(t) \end{bmatrix} + \begin{bmatrix} B \\ I \end{bmatrix} \Delta u(t) \\ y(t) = \begin{bmatrix} C & 0 \end{bmatrix} \begin{bmatrix} x(t) \\ x_u(t) \end{bmatrix}$$

• Again a linear system with states  $x(t), x_u(t)$  and input  $\Delta u(t)$ 

# LINEAR MPC - TRACKING

• Optimal control problem (quadratic performance index):

$$\min_{z} \sum_{k=0}^{N-1} \|W^{y}(y_{k+1} - r(t))\|_{2}^{2} + \|W^{\Delta u}\Delta u_{k}\|_{2}^{2} \\ [\Delta u_{k} \triangleq u_{k} - u_{k-1}], \ u_{-1} = u(t-1) \\ \text{s.t.} \quad u_{\min} \le u_{k} \le u_{\max}, \ k = 0, \dots, N-1 \\ y_{\min} \le y_{k} \le y_{\max}, \ k = 1, \dots, N \\ \Delta u_{\min} \le \Delta u_{k} \le \Delta u_{\max}, \ k = 0, \dots, N-1 \\ \ \end{array} \right| \qquad z = \begin{bmatrix} \Delta u_{0} \\ \Delta u_{1} \\ \vdots \\ \Delta u_{N-1} \end{bmatrix} \text{ or } z = \begin{bmatrix} u_{0} \\ u_{1} \\ \vdots \\ \Delta u_{N-1} \end{bmatrix}$$

weight  $W^{(\cdot)}$  = diagonal matrix, or Cholesky factor of  $Q^{(\cdot)} = (W^{(\cdot)})' W^{(\cdot)}$ 

$$\begin{array}{c|c} \min_{z} & J(z, x(t)) = \frac{1}{2}z'Hz + [x'(t)\,r'(t)\,u'(t-1)]F'z \\ \text{s.t.} & Gz \le W + S \begin{bmatrix} x(t) \\ r(t) \\ u(t-1) \end{bmatrix} \end{array} \begin{array}{c} \text{convex} \\ \text{Quadratic} \\ \text{Program} \end{array}$$

• Add the extra penalty  $\|W^u(u_k - u_{ref}(t))\|_2^2$  to track input references

• Constraints may depend on r(t), such as  $e_{\min} \leq y_k - r(t) \leq e_{\max}$ 

### LINEAR MPC TRACKING EXAMPLE

• System: 
$$y(t) = \frac{1}{s^2 + 0.4s + 1}u(t)$$

(or equivalently 
$$\frac{d^2y}{dt^2} + 0.4\frac{dy}{dt} + y = u$$
)

• Sampling with period  $T_s = 0.5$  s:

$$\begin{cases} x(t+1) &= \begin{bmatrix} 1.597 & -0.8187 \\ 1 & 0 \end{bmatrix} x(t) + \begin{bmatrix} 0.5 \\ 0 \end{bmatrix} u(t) \\ y(t) &= \begin{bmatrix} 0.2294 & 0.2145 \end{bmatrix} x(t) \end{cases}$$

#### gotodemolinear/example3.m(HybridToolbox)





#### LINEAR MPC TRACKING EXAMPLE

• Performance index:

$$\min \sum_{k=0}^{9} (y_{k+1} - r(t))^2 + 0.04\Delta u_k^2$$



• Closed-loop MPC results:





# LINEAR MPC TRACKING EXAMPLE

• Impose constraint  $0.8 \le u(t) \le 1.2$  (amplitude)



• Impose instead constraint  $-0.2 \le \Delta u(t) \le 0.2$  (slew-rate)



# **MEASURED DISTURBANCES**

• Measured disturbance v(t) = input that is measured but not manipulated

$$\begin{cases} x_{k+1} = Ax_k + Bu_k + B_v v(t) \\ y_k = Cx_k + D_v v(t) \\ x_k = A^k x_0 + \sum_{j=0}^{k-1} A^j Bu_{k-1-j} + A^j B_v v(t) \end{cases} \qquad u(t) \xrightarrow[variables]{\text{manipulated}} v(t) \xrightarrow[disturbances]{\text{manipulated}} v(t) \xrightarrow[disturbances]{\text{manipulated}$$

• Same performance index, same constraints. We still have a QP:

$$\min_{z} \quad \frac{1}{2}z'Hz + [x'(t) r'(t) u'(t-1) v'(t)]F'z \\ \text{s.t.} \quad Gz \le W + S \begin{bmatrix} x(t) \\ r(t) \\ u(t-1) \\ v(t) \end{bmatrix}$$

• Note that MPC naturally provides feedforward action on v(t) and r(t)

# **ANTICIPATIVE ACTION (A.K.A. "PREVIEW")**

$$\min_{z} \sum_{k=0}^{N-1} \|W^{y}(y_{k+1} - r(t+k))\|_{2}^{2} + \|W^{\Delta u} \Delta u(k)\|_{2}^{2}$$

• Reference not known in advance (causal):



• Future refs (partially) known in advance (anticipative action):



go to demo mpcpreview.m (MPC Toolbox)

• Same idea also applies for preview of measured disturbances v(t+k)

#### **EXAMPLE: CASCADED MPC**

- We can use preview also to coordinate multiple MPC controllers
- Example: cascaded MPC



MPC #1 sends current and future references to MPC #2

#### **EXAMPLE: DECENTRALIZED MPC**

• Example: decentralized MPC



• Commands generated by MPC #1 are measured dist. in MPC#2, and vice versa

# **SOFT CONSTRAINTS**

Relax output constraints to prevent QP infeasibility

$$\min_{z} \sum_{k=0}^{N-1} \|W^{y}(y_{k+1} - r(t))\|_{2}^{2} + \|W^{\Delta u}\Delta u_{k}\|_{2}^{2} + \|W^{u}(u_{k} - u_{ref}(t))\|_{2}^{2} + \rho_{\epsilon}\epsilon^{2}$$
s.t. 
$$x_{k+1} = Ax_{k} + Bu_{k}, \ k = 0, \dots, N-1$$

$$u_{min} \leq u_{k} \leq u_{max}, \ k = 0, \dots, N-1$$

$$\Delta u_{min} \leq \Delta u_{k} \leq \Delta u_{max}, \ k = 0, \dots, N-1$$

$$y_{min} - \epsilon V_{min} \leq y_{k} \leq y_{max} + \epsilon V_{max}, \ k = 1, \dots, N$$

$$z = \begin{bmatrix} \Delta u(0) \\ \vdots \\ \Delta u(N-1) \end{bmatrix}$$

- $\epsilon$  = "panic" variable, with weight  $\rho_{\epsilon} \gg W^y, W^{\Delta u}$
- $V_{\min}, V_{\max}$  = vectors with entries > 0. The larger the *i*-th entry of vector V, the relatively softer the corresponding *i*-th constraint
- Infeasibility can be due to:
  - modeling errors, disturbances
  - wrong MPC setup (e.g., prediction horizon is too short)

# **DELAYS - METHOD #1**

• Linear model with delays

$$\begin{array}{rcl} x(t+1) &=& Ax(t)+Bu(t-\tau)\\ y(t) &=& Cx(t) \end{array}$$



• Map delays to poles in z = 0:

$$\begin{aligned} x_k(t) &\triangleq u(t-k) \quad \Rightarrow \quad x_k(t+1) = x_{k-1}(t), \ k = 1, \dots, \tau \\ \begin{bmatrix} x_{\tau_{\tau}} \\ x_{\tau^{-1}} \\ \vdots \\ x_1 \end{bmatrix} (t+1) = \begin{bmatrix} A & B & 0 & 0 & \dots & 0 \\ 0 & 0 & I_m & 0 & \dots & 0 \\ 0 & 0 & 0 & I_m & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots & \vdots \\ 0 & 0 & 0 & 0 & \dots & 0 \end{bmatrix} \begin{bmatrix} x_{\tau_{\tau}} \\ x_{\tau^{-1}} \\ \vdots \\ x_1 \end{bmatrix} (t) + \begin{bmatrix} 0 \\ 0 \\ 0 \\ \vdots \\ I_m \end{bmatrix} u(t) \end{aligned}$$

- Apply MPC to the extended system
- Note: the prediction horizon N must be  $\geq \tau$ , otherwise no input  $u_0, \ldots, u_{N-1}$  has an effect on the output!

# **DELAYS - METHOD #2**

- Linear model with delays:  $\begin{cases} x(t+1) &= Ax(t) + Bu(t-\tau) \\ y(t) &= Cx(t) \end{cases}$
- Delay-free model:  $\bar{x}(t) \triangleq x(t+\tau) \implies \begin{cases} \bar{x}(t+1) = A\bar{x}(t) + Bu(t) \\ \bar{y}(t) = C\bar{x}(t) \end{cases}$
- Design MPC for delay-free model,  $u(t) = f_{\mathrm{MPC}}(\bar{x}(t))$
- Compute the predicted state

$$\bar{x}(t) = \hat{x}(t+\tau) = A^{\tau}x(t) + \sum_{j=0}^{\tau-1} A^j B \underbrace{u(t-1-j)}_{\text{past inputs}}$$

- Compute the MPC control move  $u(t) = f_{MPC}(\hat{x}(t+\tau))$
- For better closed-loop performance and improved robustness,  $\hat{x}(t+\tau)$  can be computed by a more complex model than (A,B,C)

# **GOOD MODELS FOR (MPC) CONTROL**

- Computation complexity depends on chosen prediction model
- Good models for MPC must be
  - Descriptive enough to capture the most significant dynamics of the system



- Simple enough for solving the optimization problem

"Things should be made as simple as possible, but not any simpler."



Albert Einstein (1879–1955)

# **MPC THEORY**

- After the industrial success of MPC, a lot of research done:
  - **linear** MPC  $\Rightarrow$  linear prediction model
  - nonlinear MPC  $\Rightarrow$  nonlinear prediction model
  - robust MPC  $\Rightarrow$  uncertain (linear) prediction model
  - stochastic MPC  $\Rightarrow$  stochastic prediction model
  - distributed/decentralized MPC⇒ multiple MPCs cooperating together
  - economic MPC  $\Rightarrow$  MPC based on arbitrary (economic) performance indices
  - hybrid MPC  $\Rightarrow$  prediction model integrating logic and dynamics
  - explicit MPC  $\Rightarrow$  offline (exact/approximate) computation of MPC
  - solvers for MPC  $\Rightarrow$  online numerical algorithms for solving MPC problems
  - data-driven MPC  $\Rightarrow$  machine learning methods tailored to MPC design
- Main theoretical issues: feasibility, stability, solution algorithms (Mayne, 2014)

# FEASIBILITY

$$\min_{z} \sum_{k=0}^{N-1} \|W^{y}(y_{k+1} - r(t))\|^{2} + \|W^{\Delta u}\Delta u_{k}\|^{2}$$
subj. to 
$$u_{\min} \leq u_{k} \leq u_{\max}, \ k = 0, \dots, N-1$$

$$y_{\min} \leq y_{k} \leq y_{\max}, \ k = 1, \dots, N$$

$$\Delta u_{\min} \leq \Delta u_{k} \leq \Delta u_{\max}, \ k = 0, \dots, N-1$$

$$QP \text{ problem}$$

- Feasibility: Will the QP problem be feasible at all sampling instants t?
- Input constraints only: always feasible if  $u/\Delta u$  constraints are consistent
- Hard output constraints:
  - When  $N < \infty$  there is no guarantee that the QP problem will remain feasible at all t, even in the nominal case
  - $N = \infty$  ok in the nominal case, but we have an infinite number of constraints!
  - Maximum output admissible set theory:  $N < \infty$  is enough (Gutman, Ckwikel, 1987) (Gilbert, Tan, 1991) (Chmielewski, Manousiouthakis, 1996) (Kerrigan, Maciejowski, 2000)

# PREDICTED AND ACTUAL TRAJECTORIES

• Consider predicted and actual trajectories



• Even assuming a perfect model and no disturbances, **predicted** open-loop trajectories and **actual** closed-loop trajectories can be different

# PRINCIPLE

• Special case: when the horizon is **infinite**, open-loop and closed-loop trajectories coincide





• This follows by **Bellman's principle of optimality**:

"Given the optimal sequence  $u_0^*, \ldots, u_{N-1}^*$  and the corresponding optimal trajectory  $x_0^*, \ldots, x_N^*$ , the subsequence  $u_k^*, \ldots, u_{N-1}^*$  is optimal for the subproblem on the horizon [k, N], starting from the optimal state  $x_k^*$ "



Richard Bellman (1920–1984)

# PRINCIPLE

- Let us focus on the subproblem from k to N. Clearly, the solution  $u_k^*,\ldots,u_{N-1}^*$  only depends on the initial state  $x_k^*$
- In particular, the first sample  $u_k^*$  only depends on  $x_k^*$ !
- Hence, an optimal control policy can always be computed in state-feedback form u<sup>\*</sup><sub>k</sub> = g<sub>k</sub>(x<sup>\*</sup><sub>k</sub>), k = 0,..., N - 1, which is a more robust form



• Bellman's principle holds since the dynamics are causal, i.e.,  $x_{k+1} = f_k(x_k, u_k)$ , and the cost function is separable:

$$\min_{u_0,...,u_{N-1}} \left\{ \sum_{j=0}^{N-1} \ell_j(x_j, u_j) \right\} = \min_{u_0,...,u_{k-1}} \left\{ \sum_{j=0}^{k-1} \ell_j(x_j, u_j) + \min_{u_k,...,u_{N-1}} \left\{ \sum_{j=k}^{N-1} \ell_j(x_j, u_j) \right\} \right\}$$
This is the basis of dynamic programming
$$V_k^*(x_k)$$

# **CONVERGENCE AND STABILITY**

$$\min_{z} \quad x'_{N} P x_{N} + \sum_{k=0}^{N-1} x'_{k} Q x_{k} + u'_{k} R u_{k}$$
  
s.t. 
$$u_{\min} \leq u_{k} \leq u_{\max}, \ k = 0, \dots, N-1$$
$$y_{\min} \leq C x_{k} \leq y_{\max}, \ k = 1, \dots, N$$

**QP** problem

 $Q=Q'\succeq 0, R=R'\succ 0, P=P'\succeq 0$ 

- Stability is a complex function of the model (A, B, C) and the MPC parameters  $N, Q, R, P, u_{\min}, u_{\max}, y_{\min}, y_{\max}$
- Stability constraints and weights on the terminal state  $x_N$  can be imposed over the prediction horizon to ensure stability of MPC
### **BASIC CONVERGENCE PROPERTIES**

(Keerthi, Gilbert, 1988) (Bemporad, Chisci, Mosca, 1994)

• Theorem: Let the MPC law be based on

V

$$\sum_{k=0}^{N-1} x'_k Q x_k + u'_k R u_k$$
  
s.t. 
$$\sum_{k=0}^{N-1} x'_k Q x_k + u'_k R u_k$$
$$u_{\min} \le u_k \le u_{\max}$$
$$y_{\min} \le C x_k \le y_{\max}$$
$$x_N = 0 \quad \leftarrow \text{"terminal constraint"}$$

with  $R, Q \succ 0, u_{\min} < 0 < u_{\max}, y_{\min} < 0 < y_{\max}$ . If the optimization problem is feasible at time t = 0 then

$$\lim_{t \to \infty} x(t) = 0, \quad \lim_{t \to \infty} u(t) = 0$$

and the constraints are satisfied at all time  $t \ge 0$ , for all  $R, Q \succ 0$ .

Many more convergence and stability results exist (Mayne, 2014)

# **CONVERGENCE PROOF**

<u>Proof:</u> Main idea = use the value function  $V^*(x(t))$  as a Lyapunov-like function

- Let  $z_t = [u_0^t \ \dots \ u_{N-1}^t]'$  be the optimal control sequence at time t
- By construction  $\bar{z}_{t+1} = [u_1^t \ \dots \ u_{N-1}^t \ 0]'$  is a feasible sequence at time t+1
- The cost of  $\bar{z}_{t+1}$  is  $V^*(x(t)) x'(t)Qx(t) u'(t)Ru(t) \ge V^*(x(t+1))$
- $V^*(x(t))$  is monotonically decreasing and  $\geq 0$ , so  $\exists \lim_{t \to \infty} V^*(x(t)) \triangleq V_{\infty}$
- Hence  $0 \leq x'(t)Qx(t) + u'(t)Ru(t) \leq V^*(x(t)) V^*(x(t+1)) \to 0 \text{ for } t \to \infty$
- Since  $R, Q \succ 0$ ,  $\lim_{t \to \infty} x(t) = 0$ ,  $\lim_{t \to \infty} u(t) = 0$

Reaching the global optimum exactly is not needed to prove convergence

# **MORE GENERAL CONVERGENCE RESULT - OUTPUT WEIGHTS**

(Keerthi, Gilbert, 1988) (Bemporad, Chisci, Mosca, 1994)

• Theorem: Consider the MPC control law based on optimizing

$$V^{*}(x(t)) = \min \qquad \sum_{k=0}^{N-1} y'_{k}Q_{y}y_{k} + u'_{k}Ru_{k}$$
  
s.t. 
$$x_{k+1} = Ax_{k} + Bu_{k}$$
$$y_{k} = Cx_{k}$$
$$u_{\min} \leq u_{k} \leq u_{\max}$$
$$y_{\min} \leq y_{k} \leq y_{\max}$$
either  $N = \infty$  or  $x_{N} = 0$ 

If the optimization problem is feasible at time t=0 then for all  $R=R'\succ 0,$   $Q_y=Q'_y\succ 0$ 

$$\lim_{t \to \infty} y(t) = 0, \quad \lim_{t \to \infty} u(t) = 0$$

and the constraints are satisfied at all time  $t \ge 0$ . Moreover, if (C, A) is a

detectable pair then  $\lim_{t\to\infty} x(t) = 0$ .

### **CONVERGENCE PROOF**

Proof:

• The shifted optimal sequence  $\bar{z}_{t+1} = [u_1^t \dots u_{N-1}^t 0]'$  (or  $\bar{z}_{t+1} = [u_1^t u_2^t \dots]'$  in case  $N = \infty$ ) is feasible sequence at time t + 1 and has cost

$$V^*(x(t)) - y'(t)Q_y y(t) - u'(t)Ru(t) \ge V^*(x(t+1))$$

- Therefore, by convergence of  $V^*(x(t))$ , we have that

$$0 \le y'(t)Q_y y(t) + u'(t)Ru(t) \le V^*(x(t)) - V^*(x(t+1)) \to 0$$

for  $t \to \infty$ 

- Since  $R, Q_y \succ 0$ , also  $\lim_{t \to \infty} y(t) = 0$ ,  $\lim_{t \to \infty} u(t) = 0$
- For all  $k = 0, \ldots, n-1$  we have that

$$0 = \lim_{t \to \infty} y'(t+k)Q_y y(t+k) = \lim_{t \to \infty} \|LC(A^k x(t) + \sum_{j=0}^{k-1} A^j Bu(t+k-1-j))\|_2^2$$

where  $Q_y = L'L$  (Cholesky factorization) and L is nonsingular

# **CONVERGENCE PROOF (CONT'D)**

- As  $u(t) \to 0$ , also  $LCA^k x(t) \to 0$ , and since L is nonsingular  $CA^k x(t) \to 0$  too, for all  $k = 0, \dots, n-1$
- Hence  $\Theta x(t) \rightarrow 0$ , where  $\Theta$  is the observability matrix of (C, A)
- If (C, A) is observable then  $\Theta$  is nonsingular and hence  $\lim_{t\to\infty} x(t) = 0$
- If (C, A) is only detectable, we can make a canonical observability decomposition and show that the observable states converge to zero
- As also  $u(t) \to 0$  and the unobservable subsystem is asymptotically stable, the unobservable states must converge to zero asymptotically too

#### **EXTENSION TO REFERENCE TRACKING**

• We want to track a constant reference r. Assume  $x_r$  and  $u_r$  exist such that

 $x_r = Ax_r + Bu_r$  (equilibrium state/input)  $r = Cx_r$ 

- Formulate the MPC problem (assume  $u_{\min} < u_r < u_{\max}, y_{\min} < r < y_{\max}$ )

$$\min \sum_{k=0}^{N-1} (y_k - r)' Q_y (y_k - r) + (u_k - u_r)' R(u_k - u_r)$$
  
s.t. 
$$x_{k+1} = Ax_k + Bu_k$$
$$u_{\min} \le u_k \le u_{\max}, \quad y_{\min} \le Cx_k \le y_{\max}$$
$$x_N = x_r$$

- We can repeat the convergence proofs in the shifted-coordinates  $x_{k+1} x_r = A(x_k x_r) + B(u_k u_r), y_k r = C(x_k x_r)$
- **Drawback**: the approach only works well in nominal conditions, as the input reference  $u_r$  depends on A, B, C (inverse static model)

1.	No stability constraint, infinite prediction horizon	$N  ightarrow \infty$
	(Keerthi, Gilbert, 1988) (Rawlings, Muske, 1993) (Bemporad, Chisci, Mosca, 1994)	
2.	End-point constraint	$x_N = 0$
	(Kwon, Pearson, 1977) (Keerthi, Gilbert, 1988) (Bemporad, Chisci, Mosca, 1994)	
3.	Relaxed terminal constraint	$x_N \in \Omega$
	(Scokaert, Rawlings, 1996)	
4.	Contraction constraint $  x_{k+1}   \le \alpha   x(t)  $	$\ , \alpha < 1$
	(Polak, Yang, 1993) (Bemporad, 1998)	
	All the proofs in (1,2,3) use the value function $V^*(x(t)) = \min_z J(z,x(t))$ as a Lyapunov function.	

# **CONTROL AND CONSTRAINT HORIZONS**

$$\min_{z} \qquad \sum_{k=0}^{N-1} \|W^{y}(y_{k} - r(t))\|_{2}^{2} + \|W^{\Delta u} \Delta u_{k}\|_{2}^{2} + \rho_{\epsilon} \epsilon^{2}$$

subj. to 
$$u_{\min} \leq u_k \leq u_{\max}, k = 0, \dots, N-1$$
  
 $\Delta u_{\min} \leq \Delta u_k \leq \Delta u_{\max}, k = 0, \dots, N-1$   
 $\Delta u_k = 0, k = N_u, \dots, N-1$   
 $y_{\min} - \epsilon V_{\min} \leq y_k \leq y_{\max} + \epsilon V_{\max}, k = 1, \dots, N_d$ 

- The input horizon N<sub>u</sub> limits the number of free variables
  - Reduced performance
  - Reduced computation time typically  $N_u = 1 \div 5$



- The constraint horizon  $N_c$  limits the number of constraints
  - Higher chance of violating output constraints but reduced computation time
- Other variable-reduction methods exist (Bemporad, Cimini, 2020)

# MPC AND LINEAR QUADRATIC REGULATION (LQR)

• Special case:  $J(z, x_0) = x'_N P x_N + \sum_{k=0}^{N-1} x'_k Q x_k + u'_k R u_k$ ,  $N_u = N$ , with matrix P solving the Discrete Algebraic Riccati Equation

$$P = A'PA - A'PB(B'PB + R)^{-1}B'PA + Q$$



Jacopo Francesco Riccati (1676–1754)

(unconstrained) MPC = LQR for any choice of the prediction horizon N

<u>Proof:</u> Easily follows from Bellman's principle of optimality (dynamic programming):  $x'_N Px_N$  = optimal "cost-to-go" from time N to  $\infty$ .

# **MPC AND CONSTRAINED LQR**

Consider again the constrained MPC law based on minimizing

$$\min_{z} \quad x'_{N} P x_{N} + \sum_{k=0}^{N-1} x'_{k} Q x_{k} + u'_{k} R u_{k}$$
  
s.t. 
$$u_{\min} \leq u_{k} \leq u_{\max}, \ k = 0, \dots, N-1$$
$$y_{\min} \leq y_{k} \leq y_{\max}, \ k = 1, \dots, N$$
$$u_{k} = K x_{k}, \ k = N_{u}, \dots, N-1$$

• Choose matrix  ${\cal P}$  and terminal gain  ${\cal K}$  by solving the LQR problem

$$K = -(R + B'PB)^{-1}B'PA$$
  

$$P = (A + BK)'P(A + BK) + K'RK + Q$$

• In a polyhedral region around the origin, **constrained MPC** = **constrained LQR** for any choice of the prediction and control horizons *N*, *N*<sub>u</sub>

(Sznaier, Damborg, 1987) (Chmielewski, Manousiouthakis, 1996) (Scokaert, Rawlings, 1998) (Bemporad, Morari, Dua Pistikopoulos, 2002)

• The larger the horizon N, the larger the region where  $\mathsf{MPC}\equiv\mathsf{constrained}\,\mathsf{LQR}$ 

#### **MPC AND CONSTRAINED LQR**

• Some MPC formulations also include the terminal constraint  $x_N \in \mathcal{X}_\infty$ 

$$\mathcal{X}_{\infty} = \left\{ x : \begin{bmatrix} u_{\min} \\ y_{\min} \end{bmatrix} \le \begin{bmatrix} K \\ C \end{bmatrix} (A + BK)^k x \le \begin{bmatrix} u_{\max} \\ y_{\max} \end{bmatrix}, \, \forall k \ge 0 \right\}$$

that is the maximum output admissible set for the closed-loop system (A + BK, B, C) and constraints  $u_{\min} \leq Kx \leq u_{\max}, y_{\min} \leq Cx \leq y_{\max}$ 

- This makes MPC  $\equiv$  constrained LQR where the MPC problem is feasible
- Recursive feasibility in ensured by the terminal constraint for all x(0) such that the MPC problem is feasible @t = 0
- The domain of feasibility may be reduced because of the additional constraint



#### Linearized model:

$$\begin{cases} \dot{x} = \begin{bmatrix} -0.0151 - 60.5651 & 0 & -32.174 \\ -0.0001 & -1.3411 & 0.9929 & 0 \\ 0.00018 & 43.2541 & -0.86939 & 0 \\ 0 & 0 & 1 & 0 \end{bmatrix} x + \begin{bmatrix} -2.516 & -13.136 \\ -0.1689 & -0.2514 \\ -17.251 & -1.5766 \\ 0 & 0 \end{bmatrix} u \\ y = \begin{bmatrix} 0 & 1 & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 1 \end{bmatrix} x \qquad (Kapasouris, Athans, Stein, 1988)$$

- Inputs: elevator and flaperon (=flap+aileron) angles
- Outputs: attack and pitch angles
- Sampling time:  $T_s = 0.05 \operatorname{sec} (+ \operatorname{ZOH})$
- Constraints:  $\pm 25^\circ$  on both angles
- Open-loop unstable, poles are −7.6636, -0.0075 ± 0.0556*j*, 5.4530

go to demo linear/afti16.m (Hybrid Toolbox)
see also mpcaircraft.m (MPC Toolbox)



#### **EXAMPLE: AFTI-F16 AIRCRAFT**

- Prediction horizon  ${\cal N}=10,$  control horizon  ${\cal N}_u=2$
- Input weights  $W^{\Delta u} = \left[ \begin{smallmatrix} 0.1 & 0 \\ 0 & 0.1 \end{smallmatrix} 
  ight], W^u = 0$
- Input constraints  $u_{\min} = -u_{\max} = \begin{bmatrix} 25^{\circ} \\ 25^{\circ} \end{bmatrix}$



#### **EXAMPLE: AFTI-F16 AIRCRAFT**

• Add output constraints  $y_{1,\min} = -y_{1,\max} = 0.5^{\circ}$ 



• Soft output constraint = convex penalty with dead zone

min  $\rho_{\epsilon} \epsilon^2$ s.t.  $y_{1,\min} - \epsilon V_{1,\min} \le y_1 \le y_{1,\max} - \epsilon V_{1,\max}$ 



#### **EXAMPLE: AFTI-F16 AIRCRAFT**

• Linear control (=unconstrained MPC) + input clipping









#### Saturation needs to be considered in the control design!

# SATURATION

• Saturation is dangerous because it can break the control loop



MPC takes saturation into account and handles it automatically (and optimally)



#### **TUNING GUIDELINES**

$$\min_{\Delta U} \sum_{k=0}^{N-1} \| W^{y}(y_{k+1} - r(t)) \|_{2}^{2} + \| W^{\Delta u} \Delta u_{k} \|_{2}^{2} + \rho_{\epsilon} \epsilon^{2}$$
subj. to 
$$\Delta u_{\min} \leq \Delta u_{k} \leq \Delta u_{\max}, \ k = 0, \dots, N_{u} - 1$$

$$\Delta u_{k} = 0, \ k = N_{u}, \dots, N - 1$$

$$u_{\min} \leq u_{k} \leq u_{\max}, \ k = 0, \dots, N_{u} - 1$$

$$y_{\min} - \epsilon V_{\min} \leq y_{k} \leq y_{\max} + \epsilon V_{\max}, \ k = 1, \dots, N_{c}$$

- weights: the larger the ratio  $W^y/W^{\Delta u}$  the more aggressive the controller
- input horizon: the larger  $N_u$ , the more "optimal" but more complex the controller
- prediction horizon: the smaller *N*, the more aggressive the controller
- constraints horizon: the smaller N<sub>c</sub>, the simpler the controller
- limits: controller less aggressive if  $\Delta u_{\min}, \Delta u_{\max}$  are small
- penalty  $\rho_{\epsilon}$ : pick up smallest  $\rho_{\epsilon}$  that keeps soft constraints reasonably satisfied

#### Always try to set $N_u$ as small as possible!

#### **TUNING GUIDELINES - EFFECT OF SAMPLING TIME**

- Let T<sub>s</sub> = sampling time used in MPC predictions
- For predicting  $T_p$  time units in the future we must set



• Slew-rate constraints  $\dot{u}_{\min} \leq rac{du}{dt} \leq \dot{u}_{\max}$  on actuators are related to  $T_s$  by

# **TUNING GUIDELINES - EFFECT OF SAMPLING TIME**

• The MPC cost to minimize can be thought in continuous-time as

$$\begin{split} J &= \int_0^{T_p} \left( \|W^y(y(\tau) - r)\|_2^2 + \|W^u(u(\tau) - u_r)\|_2^2 + \|W^{\dot{u}}\dot{u}(\tau)\|_2^2 \right) d\tau + \rho_\epsilon \epsilon^2 \\ &\approx T_s \left( \sum_{k=0}^{N-1} \|W^y(y_{k+1} - r)\|_2^2 + \|W^u(u_k - u_r)\|_2^2 + \|\underbrace{W^{\dot{u}}T_s^{-1}}_{W^{\Delta u}} \Delta u_k\|_2^2 + \rho_\epsilon T_s^{-1} \epsilon^2 \right) \end{split}$$

• Hence, when changing the sampling time from  $T_1$  to  $T_2$ , can can keep the same MPC cost function by leaving  $W^y$ ,  $W^u$  unchanged and simply rescaling

$$W_2^{\Delta u} = \frac{W^{\dot{u}}}{T_2} = \frac{T_1}{T_2} \frac{W^{\dot{u}}}{T_1} = \frac{T_1}{T_2} W_1^{\Delta u} \qquad \rho_{\epsilon 2} = \frac{\rho_{\epsilon}}{T_2} = \frac{T_1}{T_2} \frac{\rho_{\epsilon}}{T_1} = \frac{T_1}{T_2} \rho_{\epsilon 1}$$

- Note:  $T_s$  used for controller execution can be  $\neq$  than  $T_s$  used in prediction
- Small controller  $T_s \Rightarrow$  fast reaction to set-point changes / disturbances

#### SCALING

- Humans think infinite precision ...computers do not !
- Numerical difficulties may arise if variables assume very small/large values
- Example:

$$\begin{array}{ll} y_1 \in [-1e-4, 1e-4] & [\mathsf{V}] \\ y_2 \in [-1e4, 1e4] & [\mathsf{Pa}] \end{array} \begin{array}{ll} y_1 \in [-0.1, 0.1] & [\mathsf{mV}] \\ y_2 \in [-10, 10] & [\mathsf{kPa}] \end{array}$$

- Ideally all variables should be in [-1,1]. For example, one can replace y with  $y/y_{\rm max}$
- Scaling also possible after formulating the QP problem (=preconditioning)

# **PRE-STABILIZATION OF OPEN-LOOP UNSTABLE MODELS**

- Numerical issues may arise with open-loop unstable models
- When condensing the QP we substitute  $x_k = A^k x_0 + \sum_{j=0}^{n-1} A^j B u_{k-1-j}$  that

may lead to a badly conditioned Hessian matrix H

$$H = \begin{bmatrix} B & 0 & \dots & 0 \\ AB & B & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ A^{N-1}B & A^{N-2}B & \dots & B \end{bmatrix}' \begin{bmatrix} Q & 0 & 0 & \dots & 0 \\ 0 & Q & 0 & \dots & 0 \\ \vdots & \ddots & \ddots & \vdots \\ 0 & \dots & 0 & Q & 0 \\ 0 & 0 & \dots & 0 & P \end{bmatrix} \begin{bmatrix} B & 0 & \dots & 0 \\ AB & B & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ A^{N-1}B & A^{N-2}B & \dots & B \end{bmatrix} + \begin{bmatrix} R & 0 & \dots & 0 \\ 0 & R & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & \dots & 0 & R \end{bmatrix}$$

- **Pre-stabilizing** the system with  $u_k = Kx_k + v_k$  leads to  $x_{k+1} = A_K x_k + Bv_k$ ,  $A_K \triangleq A + BK$ , and therefore  $x_k = A_K^k x_0 + \sum_{j=0}^{k-1} A_K^j Bv_{k-1-j}$
- Input constraints become mixed constraints  $u_{\min} \leq K x_k + v_k \leq u_{\max}$
- K can be chosen for example by pole-placement or LQR

# **OBSERVER DESIGN FOR MPC**

# **STATE OBSERVER FOR MPC**



- Full state x(t) of process may not be available, only outputs y(t)
- Even if x(t) is available, noise should be filtered out
- Prediction and process models may be quite different
- The state x(t) may not have any physical meaning (e.g., in case of model reduction or subspace identification)

We need to use a state observer

• Example: Luenberger observer  $\hat{x}(t+1) = A\hat{x}(t) + Bu(t) + L(y(t) - C\hat{x}(t))$ 

# **EXTENDED MODEL FOR OBSERVER DESIGN**



unmeasured disturbance model

$$\begin{aligned} x_d(t+1) &= \bar{A}x_d(t) + \bar{B}n_d(t) \\ d(t) &= \bar{C}x_d(t) + \bar{D}n_d(t) \end{aligned}$$

#### measurement noise model

$$\begin{cases} x_m(t+1) = \tilde{A}x_m(t) + \tilde{B}n_m(t) \\ m(t) = \tilde{C}x_m(t) + \tilde{D}n_m(t) \end{cases}$$

- Note: the measurement noise model is not used for optimization, as we want  $z_m$  to go to its reference, not  $y_m$ 

4

• Plant model

$$\begin{cases} x(t+1) = Ax(t) + B_u u(t) + B_v v(t) + B_d d(t) \\ y(t) = Cx(t) + D_v v(t) + D_d d(t) \end{cases}$$

W.

• Full model for designing Kalman filter

Rudolf Emil Kalman (1930–2016)

$$\begin{bmatrix} x(t+1) \\ x_d(t+1) \\ x_m(t+1) \end{bmatrix} = \begin{bmatrix} AB_d \bar{C} & 0 \\ 0 & \bar{A} & 0 \\ 0 & 0 & \bar{A} \end{bmatrix} \begin{bmatrix} x(t) \\ x_d(t) \\ x_m(t) \end{bmatrix} + \begin{bmatrix} B_u \\ 0 \\ 0 \end{bmatrix} u(t) + \begin{bmatrix} B_v \\ 0 \\ 0 \end{bmatrix} v(t) + \begin{bmatrix} B_u \\ 0 \\ 0 \end{bmatrix} n_d(t) + \begin{bmatrix} 0 \\ \bar{B} \\ 0 \end{bmatrix} n_m(t) + \begin{bmatrix} B_u \\ 0 \\ 0 \end{bmatrix} n_u(t)$$

$$y_m(t) = \begin{bmatrix} C_m & D_{dm} \bar{C} & \bar{C} \end{bmatrix} \begin{bmatrix} x(t) \\ x_d(t) \\ x_m(t) \end{bmatrix} + D_{vm}v(k) + \bar{D}_m n_d(t) + \bar{D}_m n_m(t)$$

- $n_d(k)$  = source of modeling errors
- $n_m(k)$  = source of measurement noise
- $n_u(k)$  = white noise on input u (added to compute the Kalman gain)

# **OBSERVER IMPLEMENTATION**

• Measurement update

$$\hat{y}_m(t|t-1) = C_m \hat{x}(t|t-1)$$
$$\hat{x}(t|t) = \hat{x}(t|t-1) + M(y_m(t) - \hat{y}_m(t|t-1))$$

• Time update

$$\hat{x}(t+1|t) = A\hat{x}(t|t-1) + Bu(t) + L(y_m(t) - \hat{y}_m(t|t-1))$$

- Note that if L = AM then  $\hat{x}(t+1|t) = A\hat{x}(t|t) + Bu(t)$
- The separation principle holds (under certain assumptions)

(Muske, Meadows, Rawlings, 1994)

# **I/O FEEDTHROUGH**

• We always assumed no feedthrough from u to measured y

$$y_k = Cx_k + Du_k + D_v v_k + D_d d_k, \quad D_m = 0$$

- This avoids static loops between state observer, as  $\hat{x}(t|t)$  depends on u(t) via  $\hat{y}_m(t|t-1)$ , and MPC (u(t) depends on  $\hat{x}(t|t)$ )
- Often D = 0 is not a limiting assumption as
  - often actuator dynamics must be considered (*u* is the set-point to a low-level controller of the actuators)
  - most physical models described by ordinary differential equations are strictly causal, and so is the discrete-time version of the model
- In case  $D \neq 0$ , we can assume a **delay** in executing the commanded u

$$y_k = C_m x_k + D u_{k-1}$$

and treat u(t-1) as an extra state

• Not an issue for **unmeasured** outputs



# **INTEGRAL ACTION IN MPC**

# **CONSTANT DISTURBANCE MODEL**

Tracking errors in steady state can be due to model mismatch / disturbances

$$\begin{cases} x_{k+1} &= Ax_k + Bu_k \\ y_k &= Cx_k \end{cases}$$

prediction model  $\neq$  plant dynamics



• Possible remedy: introduce a constant disturbance model

$$\begin{cases} x_{k+1} = Ax_k + Bu_k \\ d_{k+1} = d_k \\ y_k = Cx_k + d_k \end{cases}$$

augmented prediction model



and estimate  $x_k, d_k$  by a state observer

# **OUTPUT INTEGRATORS AND OFFSET-FREE TRACKING**



- The state observer (e.g., a Kalman filter) estimates both  $\hat{x}(t)$  and  $\hat{d}(t)$  from y(t)
- Intuitively, we get offset-free tracking in steady-state because:
  - the observer makes  $C\hat{x}(t) + \hat{d}(t) \rightarrow y(t)$  (estimation error)
  - the MPC controller makes  $C\hat{x}(t) + \hat{d}(t) \rightarrow r(t)$  (predicted tracking error)
  - the combination of the two makes  $y(t) \rightarrow r(t)$

- (actual tracking error)
- In steady state, the term  $\hat{d}(t)$  compensates for model mismatch

# **OUTPUT INTEGRATORS AND OFFSET-FREE TRACKING**

• More general result: consider the disturbance model

$$\begin{cases} x_{k+1} = Ax_k + Bu_k + B_d d_k \\ d_{k+1} = d_k \\ y_k = Cx_k + D_d d_k \end{cases}$$

special case: output integrators  $B_d = 0, D_d = I$ 

• Theorem: (Pannocchia, Rawlings, 2003)

If # disturbances = # measured outputs, then all pairs  $(B_d, D_d)$  satisfying

$$\operatorname{rank} \left[ \begin{array}{cc} I-A & -B_d \\ C & D_d \end{array} \right] = n_x + n_y$$

guarantee zero offset in steady-state (y = r), provided that constraints are not active in steady-state and the closed-loop system is asymptotically stable

See more on survey paper (Pannocchia, Gabiccini, Artoni, 2015)

#### DISTURBANCE MODEL EXAMPLE

• Open-loop system: 
$$A = \begin{bmatrix} 1 & -1 & -2 & 1 \\ 0 & -2 & 3 & 2 \\ 0 & 2 & -1 & -1 \\ 0 & 2 & 0 & -2 \end{bmatrix}, B = \begin{bmatrix} 1 \\ 0 \\ 1 \\ 1 \end{bmatrix}, C_m = \begin{bmatrix} 1 & 1 & 0 & 0 \end{bmatrix}$$

• We cannot add an output integrator since the pair  $\left(\begin{bmatrix} A & 0 \\ 0 & 1 \end{bmatrix}, \begin{bmatrix} C & 1 \end{bmatrix}\right)$  is not observable

• Add an input integrator:  $B_d = B$ ,  $D_d = 0$ ,  $\operatorname{rank} \begin{bmatrix} A & B_d \\ C_m & D_d \end{bmatrix} = 5 = n_x + n_y$  $\begin{cases} x(t+1) &= Ax(t) + B(u(t) + d(t)) \\ d(t+1) &= d(t) \\ y(t) &= Cx(t) + 0 \cdot d(t) \end{cases}$ 

### **OVERALL OBSERVER MODEL FOR OFFSET-FREE MPC**



#### (observer model structure used in the MPC Toolbox for MATLAB)

- Idea: add the integral of the tracking error as an additional state (original idea developed for integral action in state-feedback control)
- Extended prediction model:

$$\begin{cases} x(t+1) = Ax(t) + B_u u(t) + 0 \cdot r(t) &\leftarrow r(t) \text{ is seen as a meas. disturbance} \\ q(t+1) = q(t) + \underbrace{Cx(t) - r(t)}_{\text{Tracking error}} &\leftarrow \text{ integral action} \\ y(t) = Cx(t) \end{cases}$$

- $||W^iq||_2^2$  is penalized in the cost function, otherwise it is useless.  $W^i$  is a new tuning knob
- Intuitively, if the MPC closed-loop is asymptotically stable then q(t) converges to a constant, and hence y(t) r(t) converges to zero.

# **REFERENCE / COMMAND GOVERNOR**

(Bemporad, Mosca, 1994) (Gilbert, Kolmanovsky, Tan, 1994) (Garone, Di Cairano, Kolmanovsky, 2016)



- MPC manipulates set-points to a linear feedback loop to enforce constraints
- Separation of problems:
  - Local feedback guarantees offset-free tracking  $y(t)-w(t) \to 0$  in steady-state in the absence of constraints
  - Actual reference w(t) generated by MPC to take care of constraints
- Advantages: small-signal properties preserved, fewer variables to optimize

$$w(t) = \arg \min_{w} \|w - r(t)\|_{2}^{2}$$
  
s.t.  $c_{t+k} \in C$ 

#### INTEGRAL ACTION AND $\Delta u$ -FORMULATION

• In control systems, **integral action** occurs if the controller has a transfer-function from the output to the input of the form

$$u(t) = \frac{B(z)}{(z-1)A(z)}y(t), \qquad B(1) \neq 0$$

• One may think that the  $\Delta u$ -formulation of MPC provides integral action ...

... is it true ?

• **Example**: we want to regulate the output y(t) to zero of the scalar system

$$\begin{aligned} x(t+1) &= \alpha x(t) + \beta u(t) \\ y(t) &= x(t) \end{aligned}$$
# INTEGRAL ACTION AND $\Delta u$ -FORMULATION

• Design an unconstrained MPC controller with horizon N = 1

$$\begin{aligned} \Delta u(t) &= \arg \min_{\Delta u_0} \Delta u_0^2 + \rho y_1^2 \\ \text{s.t.} \quad u_0 &= u(t-1) + \Delta u_0 \\ y_1 &= x_1 = \alpha x(t) + \beta (\Delta u_0 + u(t-1)) \end{aligned}$$

• By substitution, we get

$$\begin{aligned} \Delta u(t) &= \arg \min_{\Delta u_0} \Delta u_0^2 + \rho(\alpha x(t) + \beta u(t-1) + \beta \Delta u_0)^2 \\ &= \arg \min_{\Delta u_0} (1 + \rho \beta^2) \Delta u_0^2 + 2\beta \rho(\alpha x(t) + \beta u(t-1)) \Delta u_0 \\ &= -\frac{\beta \rho \alpha}{1 + \rho \beta^2} x(t) - \frac{\rho \beta^2}{1 + \rho \beta^2} u(t-1) \end{aligned}$$

• Since x(t) = y(t) and  $u(t) = u(t-1) + \Delta u(t)$  we get the linear controller

$$u(t)=-rac{rac{
hoetalpha}{1+
hoeta^2}z}{z-rac{1}{1+
hoeta^2}}y(t)$$
 No pole in  $z=1$ 

• Reason: MPC gives a feedback gain on both x(t) and u(t-1), not just on x(t)

# INTEGRAL ACTION AND $\Delta u$ -FORMULATION

• Numerical test (with MPC Toolbox)

```
alpha=.5;
beta=3;
sys=ss(alpha,beta,1,0);sys.ts=1;
rho=1;p=1;m=1;
weights=struct('OV',rho,'MVRate',1);
mpc1=mpc(sys,1,p,m,weights);
setoutdist(mpc1,'remove',1); % no output disturbance model
mpc1tf=tf(mpc1);
sum(mpc1tf.den{1})
ans = 0.9000
```

• Now add an output integrator as disturbance model

```
setoutdist(mpc1,'integrators'); % add output disturbance model
mpcltf=tf(mpc1);
sum(mpcltf.den{1})
ans = -6.4185e-16
```

### MPC AND INTERNAL MODEL PRINCIPLE

• Assume we have an **internal model** of the reference signal r(t)

$$\begin{aligned} x^r(t+1) &= A_r x^r(t) \\ r(t) &= C_r x^r(t) \end{aligned}$$

• Consider the augmented prediction model

$$\begin{bmatrix} x_{k+1} \\ x_{k+1}^r \end{bmatrix} = \begin{bmatrix} A & 0 \\ 0 & A_r \end{bmatrix} \begin{bmatrix} x_k \\ x_k^r \end{bmatrix} + \begin{bmatrix} B \\ 0 \end{bmatrix} u_k$$

- Design a state observer (e.g., via pole-placement) to estimate  $x(t), x^r(t)$  from  $\begin{bmatrix} y(t) \\ r(t) \end{bmatrix} = \begin{bmatrix} C & 0 \\ 0 & C_r \end{bmatrix} \begin{bmatrix} x(t) \\ x^r(t) \end{bmatrix}$
- Design an MPC controller with output  $e_k = y_k r_k = \left[ \begin{array}{c} C & -C_r \end{array} \right] \left[ \begin{array}{c} x_k \\ x_k \\ x_k \end{array} \right]$

## MPC AND INTERNAL MODEL PRINCIPLE

• Penalize 
$$\sum_{k=1}^{N} e_k^2$$
 (+small penalty on  $u^2$  or  $\Delta u^2$ )

• Set control horizon  $N_u = N$ 

• Example: 
$$r(t) = r_0 \sin(\omega t + \phi_0)$$
,  $\omega = 1$  rad/s

$$A = \begin{bmatrix} 1.6416 & -0.7668 & 0.2416 \\ 1 & 0 & 0 \\ 0 & 0.125 & 0 \end{bmatrix}$$
$$B = \begin{bmatrix} 0.5 \\ 0 \\ 0 \end{bmatrix}$$
$$C = \begin{bmatrix} 0.1349 & 0.0159 & -0.1933 \end{bmatrix}$$

$$A_r = \begin{bmatrix} 1.7552 & -1 \\ 1 & 0 \end{bmatrix}$$
$$C_r = \begin{bmatrix} .2448 & .2448 \end{bmatrix}$$

observer poles placed in  $\{0.3, 0.4, 0.5, 0.6, 0.7\}$ 

sample time  $T_s = 0.5 \, \mathrm{s}$ 

input saturation  $-2 \le u(t) \le 2$ 



# MODEL PREDICTIVE CONTROL TOOLBOX

(Bemporad, Ricker, Morari, 1998-present)

- Several MPC design features available:
  - explicit MPC

...

- time-varying/adaptive models, nonlinear models, weights, constraints
- stability/frequency analysis of closed-loop (inactive constraints)
- Prediction models can be generated by the Identification Toolbox or automatically linearized from Simulink
- Fast command-line MPC functions (compiled EML-code)
- Graphical User Interface
- Simulink library (compiled EML-code)



### **MPC SIMULINK LIBRARY**



### **MPC SIMULINK BLOCK**

### Block Parameters: MPC Controller MPC (mask) (link) The MPC Controller block lets you design and simulate a model predictive controller defined in the Model Predictive Control Toolbox. Parameters MPC Controller mpcobi Design Initial Controller State [] Review Block Options General Online Features Default Conditions Others Additional Inports Measured disturbance (md) External manipulated variable (ext.mv) Targets for manipulated variables (mv.target) Additional Outports Optimal cost (cost) Optimal control sequence (mv.seq) Optimization status (qp.status) Optimal state sequence (x.seq) Estimated controller states (est.state) Optimal output sequence (v.seq) State Estimation Use custom state estimation instead of using the built-in Kalman filter (x[k]k]) ОК Cancel Help



### **MPC SIMULINK BLOCK**

### Block Parameters: MPC Controller MPC (mask) (link) The MPC Controller block lets you design and simulate a model predictive controller defined in the Model Predictive Control Toolbox. Parameters MPC Controller mpcobj Design Initial Controller State Review **Block Options** Online Features Default Conditions Others General Constraints Lower MV limits (umin) Upper MV limits (umax) Lower OV limits (ymin) Upper OV limits (ymax) Custom constraints (E, F, G, S) Weights OV weights (y.wt) MV weights (u.wt) MVRate weights (du.wt) Slack variable weight (ecr.wt) Prediction and Control Horizons Adjust prediction horizon (p) and control horizon (m) at run time Maximum prediction horizon 10

ОК

Cancel

Help



### **MPC SIMULINK BLOCK**

### Block Parameters: MPC Controller MPC (mask) (link) The MPC Controller block lets you design and simulate a model predictive controller defined in the Model Predictive Control Toolbox. Parameters MPC Controller mpcobi Desian Initial Controller State [] Review Block Options General Online Features Default Conditions Others Signal Attributes ~: Block Data Type double >> Sample Time □ Inherit sample time (must be the same as controller sample time) **Optimization Settings** Use external signal to enable or disable optimization (switch) ОК Cancel Help Apply



### **MPC GRAPHICAL USER INTERFACE**



>> mpcDesigner

(old version: >> mpctool)

### See video on Mathworks' web site (link)

### **EXAMPLE: MPC OF A DC SERVOMOTOR**



Symbol	Value (MKS)	Meaning	>> openExample mpcmotor
$L_S \\ d_S \\ J_S \\ J_M \\ \beta_M$	1.0 0.02 negligible 0.5 0.1	shaft length shaft diameter shaft inertia motor inertia motor viscous friction coefficient	
$R \\ k_T$	20 10	resistance of armature motor constant	see also
$ ho \\ k_{ heta}$	20 1280.2	gear ratio torsional rigidity	(Llubrid Tealboy)
$J_L \ eta_L \ T_s$	50 <i>J<sub>M</sub></i> 25 0.1	nominal load inertia load viscous friction coefficient sampling time	

### **DC SERVOMOTOR MODEL**

$$\dot{x} = \begin{bmatrix} 0 & 1 & 0 & 0 \\ -\frac{k_{\theta}}{J_{L}} & -\frac{\beta_{L}}{J_{L}} & \frac{k_{\theta}}{\rho J_{L}} & 0 \\ 0 & 0 & 0 & 1 \\ \frac{k_{\theta}}{\rho J_{M}} & 0 & -\frac{k_{\theta}}{\rho^{2} J_{M}} & -\frac{\beta_{M} + k_{T}^{2} / R}{J_{M}} \end{bmatrix} x + \begin{bmatrix} 0 \\ 0 \\ 0 \\ \frac{k_{T}}{R J_{M}} \end{bmatrix} V \quad x = \begin{bmatrix} \frac{\theta_{L}}{\dot{\theta}_{L}} \\ \frac{\theta_{M}}{\dot{\theta}_{M}} \end{bmatrix}$$

$$\theta_{L} = \begin{bmatrix} 1 & 0 & 0 & 0 \end{bmatrix} x \quad y = \begin{bmatrix} \theta_{L} \\ \frac{\theta_{L}}{T} \end{bmatrix}$$

$$T = \begin{bmatrix} k_{\theta} & 0 & -\frac{k_{\theta}}{\rho} & 0 \end{bmatrix} x$$

>> [plant, tau] = mpcmotormodel;
>> plant = setmpcsignals(plant,'MV',1,'MO',1,'UO',2);

### **DC SERVOMOTOR CONSTRAINTS**

• The input DC voltage  $\boldsymbol{V}$  is bounded withing the range

 $|V| \le 220 \, V$ 

- Finite shear strength  $\tau_{adm}=50N/mm^2$  requires that the torsional torque T satisfies the constraint

 $|T| \le 78.5398 \, Nm$ 

• Sampling time of model/controller:  $T_s = 0.1s$ 

>> MV = struct('Min',-220,'Max',220);
>> OV = struct('Min',{-Inf,-78.5398},'Max',{Inf,78.5398});
>> Ts = 0.1;

### **DC SERVOMOTOR - MPC SETUP**

$$\min_{\Delta U} \sum_{k=0}^{p-1} \|W^{y}(y_{k+1} - r(t))\|^{2} + \|W^{\Delta u}\Delta u_{k}\|^{2} + \rho_{\epsilon}\epsilon^{2}$$
subj. to
$$\Delta u_{\min} \leq \Delta u_{k} \leq \Delta u_{\max}, \ k = 0, \dots, m-1$$

$$\Delta u_{k} = 0, \ k = m, \dots, p-1$$

$$u_{\min} \leq u_{k} \leq u_{\max}, \ k = 0, \dots, m-1$$

$$y_{\min} - \epsilon V_{\min} \leq y_{k} \leq y_{\max} + \epsilon V_{\max}, \ k = 1, \dots, p$$

```
>> Weights = struct('MV',0,'MVRate',0.1,'OV',[0.1 0]);
>> p = 10;
>> m = 2;
>> mpcobj = mpc(plant,Ts,p,m,Weights,MV,OV);
```

### **DC SERVOMOTOR - CLOSED-LOOP SIMULATION**



### **DC SERVOMOTOR - CLOSED-LOOP SIMULATION**



### closed-loop simulation in Simulink

```
>> mdl = 'mpc_motor';
>> open_system(mdl)
>> sim(mdl)
```

### **DC SERVOMOTOR - CLOSED-LOOP SIMULATION**



- same MPC tuning parameters
- setpoint  $r(t) = \pi \sin(0.4t) \deg$

• Take simulation model sldemo\_suspn in MATLAB



$$F_{front} = 2K_f(L_f\theta - (z+h)) + 2C_f(L_f\dot{\theta} - \dot{z}) + \boldsymbol{u_f}$$

 $F_{front}, F_{rear} =$  upward force on body from front/rear suspension  $K_f, K_r =$  front and rear suspension spring constant  $C_f, C_r =$  front and rear suspension damping rate  $L_f, L_r =$  horizontal distance from c.g. to front/rear suspension  $\theta, \dot{\theta} =$  pitch (rotational) angle and its rate of change  $z, \dot{z} =$  bounce (vertical) distance and its rate of change

- For control purposes we add external forces  $u_f$ ,  $u_r$  as manipulated variables
- The system has 4 states:  $\theta$ ,  $\dot{\theta}$ , z,  $\dot{z}$
- Measured disturbances: road height h, pitch moment from vehicle acceleration

• Step #1: get a linear discrete-time model (4 inputs, 3 outputs, 4 states)

```
>> plant_mdl = 'suspension_model';
>> op = operspec(plant_mdl);
>> [op_point, op_report] = findop(plant_mdl,op);
>> sys = linearize(plant_mdl, op_point);
>> Ts = 0.025; % sample time (s)
>> plant = c2d(sys,Ts);
>> plant = setmpcsignals(plant,'MV',[1 2],'MD',...
[3 4],'MO',[1 2],'UO',3);
```

• Step #2: design the MPC controller

```
>> dfmax = .1/.1; % [kN/s]
>> MV = struct('RateMin',-Ts*dfmax, Ts*dfmax,...
'RateMax',Ts*dfmax,Ts*dfmax);
>> OV = [];
>> Weights = struct('MV',[0 0], 'MVRate',[.01 .01],...
'OV',[.01 0 10]);
>> p = 50; % Prediction horizon
>> m = 5; % Control horizon
>> mpcobj = mpc(plant,Ts,p,m,Weights,MV,OV);
```



Closed-loop MPC results



# FREQUENCY ANALYSIS OF MPC (FOR SMALL SIGNALS)

- Unconstrained MPC gain + linear observer = linear dynamical system
- Closed-loop MPC analysis can be performed using standard frequency-domain tools (e.g., Bode plots for sensitivity analysis)



## **CONTROLLER MATCHING**

• Given a desired linear controller  $u = K_d x$ , find a set of weights Q, R, P defining an MPC problem such that

$$-\left[I\,0\,\ldots\,0\right]H^{-1}F=K_d$$

i.e., the MPC law coincides with  $K_d$  when the constraints are inactive

• Recall that the QP matrices are  $H=2(\bar{R}+\bar{S}'\bar{Q}\bar{S}), F=2\bar{S}'\bar{Q}\bar{T}$ , where

$$\bar{Q} = \begin{bmatrix} Q & 0 & 0 & \dots & 0 \\ 0 & Q & 0 & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & \dots & 0 & \bar{Q} & 0 \\ 0 & 0 & \dots & 0 & P \end{bmatrix}, \ \bar{R} = \begin{bmatrix} R & 0 & \dots & 0 \\ 0 & R & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ 0 & \dots & 0 & R \end{bmatrix}, \ \bar{S} = \begin{bmatrix} B & 0 & \dots & 0 \\ AB & B & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ A^{N-1}B & A^{N-2}B & \dots & B \end{bmatrix}, \ \bar{T} = \begin{bmatrix} A \\ A^2 \\ \vdots \\ A^N \end{bmatrix}$$

• The above inverse optimality problem can be cast to a convex problem

(Di Cairano, Bemporad, 2010)

• Result extended to match any linear controller/observer by LQR/Kalman filter

(Zanon, Bemporad, 2022)

### **CONTROLLER MATCHING - EXAMPLE**

(Di Cairano, Bemporad, 2010)

- Open-loop process: y(t) = 1.8y(t-1) + 1.2y(t-2) + u(t-1)
- Constraints:  $-24 \le u(t) \le 24$ ,  $y(t) \ge -5$
- Desired controller = PID with gains  $K_I = 0.248$ ,  $K_P = 0.752$ ,  $K_D = 2.237$

$$\begin{aligned} u(t) &= -\left(K_{I}\mathcal{I}(t) + K_{P}y(t) + \frac{K_{D}}{T_{s}}(y(t) - y(t-1))\right) \\ \mathcal{I}(t) &= \mathcal{I}(t-1) + T_{s}y(t) \end{aligned} \qquad x(t) = \begin{bmatrix} y(t-1) \\ y(t-2) \\ \mathcal{I}(t-1) \\ u(t-1) \end{bmatrix}$$

• Matching result (using inverse LQR):

$$Q^* = \begin{bmatrix} 6.401 & 0.064 & -0.001 & 0.020 \\ 0.064 & 6.605 & 0.006 & 0.080 \\ -0.001 & 0.006 & 6.647 & -0.020 \\ 0.019 & 0.080 & -0.020 & 6.378 \end{bmatrix}, R^* = 1, P^* = \begin{bmatrix} 422.7 & 241.7 & 50.39 & 201.4 \\ 241.7 & 151.0 & 32.13 & 120.4 \\ 50.39 & 32.13 & 19.85 & 26.75 \\ 201.4 & 120.4 & 26.75 & 106.6 \end{bmatrix}$$

# CONTROLLER MATCHING - EXAMPLE



 Note: This is not trivially a saturation of a PID controller. In this case saturating the PID output leads to closed-loop instability!



# LINEAR MPC BASED ON LINEAR PROGRAMMING

## LINEAR MPC BASED ON LP

(Propoi, 1963) (Bemporad, Borrelli, Morari, 2003)

- $x \in \mathbb{R}^n$ • Linear prediction model:  $\begin{cases} x_{k+1} = Ax_k + Bu_k \\ y_k = Cx_k \end{cases}$  $u \in \mathbb{R}^m$  $y \in \mathbb{R}^p$
- Constraints to enforce:

$$\begin{cases} u_{\min} \le u(t) \le u_{\max} \\ y_{\min} \le y(t) \le y_{\max} \end{cases}$$

Constrained optimal control problem ( $\infty$ -norms):  $||v||_{\infty} \triangleq \max_{i=1,\dots,n} |v_i|$ 

$$\min_{z} \|Px_{N}\|_{\infty} + \sum_{k=0}^{N-1} \|Qx_{k}\|_{\infty} + \|Ru_{k}\|_{\infty}$$
s.t.  $u_{\min} \leq u_{k} \leq u_{\max}, \ k = 0, \dots, N-1$   
 $y_{\min} \leq y_{k} \leq y_{\max}, \ k = 1, \dots, N$ 

$$R, Q, P$$
full rank
$$z = \begin{bmatrix} u_{0} \\ u_{1} \\ \vdots \\ u_{N-1} \end{bmatrix}$$

### LINEAR MPC BASED ON LP

• **Basic trick**: introduce slack variables (Q<sup>i</sup> = *i*-th row of Q)

and minimize  $\epsilon_N^x + \sum_{k=0}^{N-1} \epsilon_k^x + \epsilon_k^u$  w.r.t.  $u_0, \ldots, u_{N-1}, \epsilon_0^x, \ldots, \epsilon_N^x, \epsilon_0^u, \ldots, \epsilon_N^u$ (not that  $\epsilon_0^x$  can be eliminated as  $x_0$  is given)

• Example:  $\min_{x} |x| \to \min_{x,\epsilon} \epsilon$ s.t.  $\epsilon \ge x, \epsilon \ge -x$ At optimility,  $\epsilon^* = |x^*|$ 

## LINEAR MPC BASED ON LP

• Linear prediction model: 
$$x_k = A^k x_0 + \sum_{i=0}^{k-1} A^i B u_{k-1-i}$$

• Optimization problem:

$$V(x_0) = \min_{z} [1 \dots 10 \dots 0]z$$
 (linear objective)  
s.t.  $Gz \le W + Sx_0$  (linear constraints)

### Linear Program (LP)

- optimization vector:  $z \triangleq [\epsilon_0^u \ \dots \ \epsilon_{N-1}^u \ \epsilon_1^x \ \dots \ \epsilon_N^x \ u'_0, \dots, u'_{N-1}]' \in \mathbb{R}^{N(n_u+2)}$
- G, W, S are obtained from weights Q, R, P, and model matrices A, B, C
- Q, R, P can be selected to guarantee closed-loop stability

(Bemporad, Borrelli, Morari, 2003)

### **EXTENSION TO ARBITRARY CONVEX PWA FUNCTIONS**

### Result

Every convex piecewise affine function  $\ell : \mathbb{R}^n \to \mathbb{R}$  can be represented as the max of affine functions, and vice versa

(Schechter, 1987)

Example:  $\ell(x) = |x| = \max\{x, -x\}$ 

Constrained optimal control problem

$$\min_{U} \quad \ell_N(x_N) + \sum_{k=0}^{N-1} \ell_k(x_k, u_k)$$
  
s.t.  $g_k(x_k, u_k) \le 0, \ k = 0, \dots, N-1$   
 $g_N(x_N) \le 0$ 



 $\ell_k, \ell_N, g_k, g_N$  are arbitrary convex piecewise affine (PWA) functions

### **CONVEX PWA OPTIMIZATION PROBLEMS AND LP**

• Minimization of a convex PWA function  $\ell(x)$ :



- By construction  $\epsilon \ge \max\{a'_1x + b_1, a'_2x + b_2, a'_3x + b_3, a'_4x + b_4\}$
- · By contradiction it is easy to show that at the optimum we have that

$$\epsilon = \max\{a_1'x + b_1, a_2'x + b_2, a_3'x + b_3, a_4'x + b_4\}$$

- Convex PWA constraints  $\ell(x) \le 0$  can be handled similarly by imposing  $a_i'x+b_i \le 0, \forall i=1,2,3,4$ 

- QP- and LP-based share the same set of feasible inputs ( $Gz \le W + Sx$ )
- When constraints dominate over performance there is little difference between them (e.g., during transients)
- Small-signal response, however, is usually less smooth with LP than with QP, because in LP an optimal point is always on a vertex



 $\epsilon$  = additional slack variables introduced to represent convex PWA costs